

Microscale instability and mixing in driven and active suspensions

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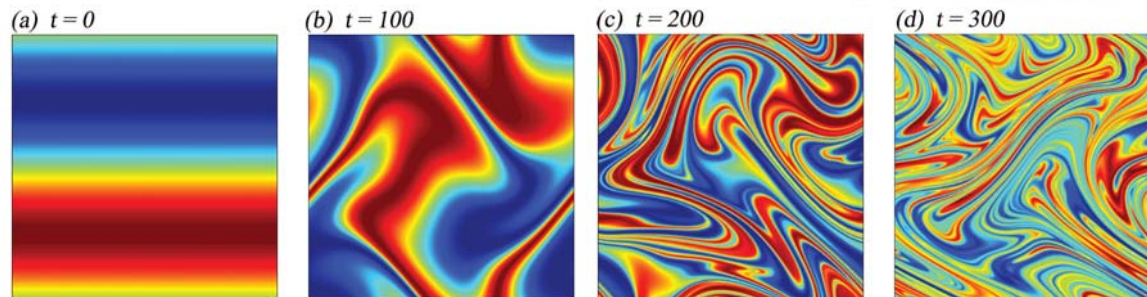
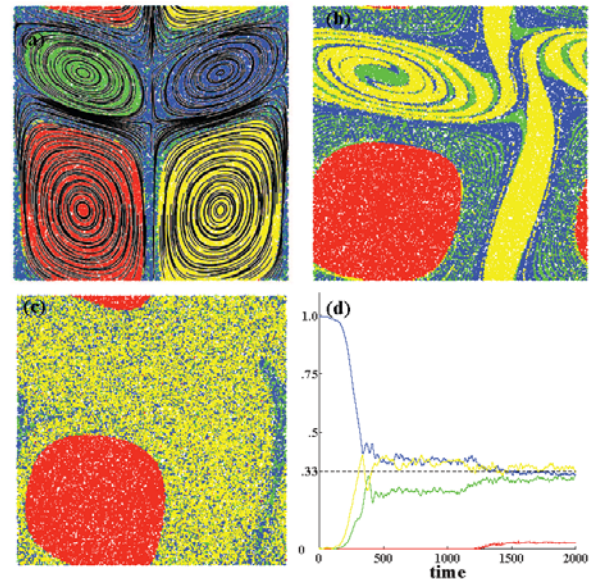
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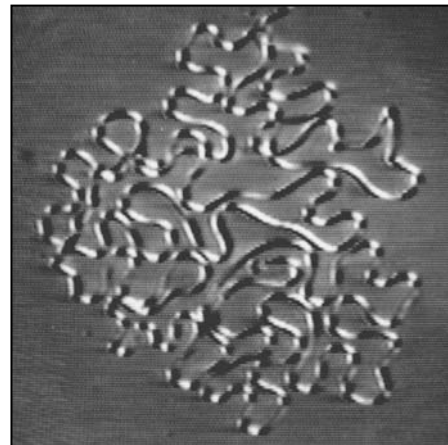


Dynamics and interactions of micro-structure in complex fluids

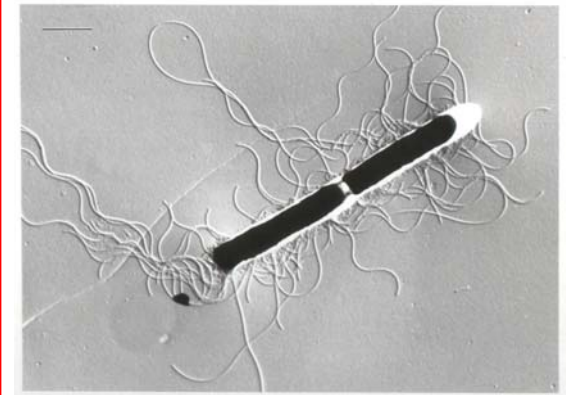
- Dynamics of non-Newtonian fluids
- Reinforced composite materials
- Biological locomotion
- Elastic “turbulence” & low Re mixing

Groisman & Sternberg '00, '01, ...

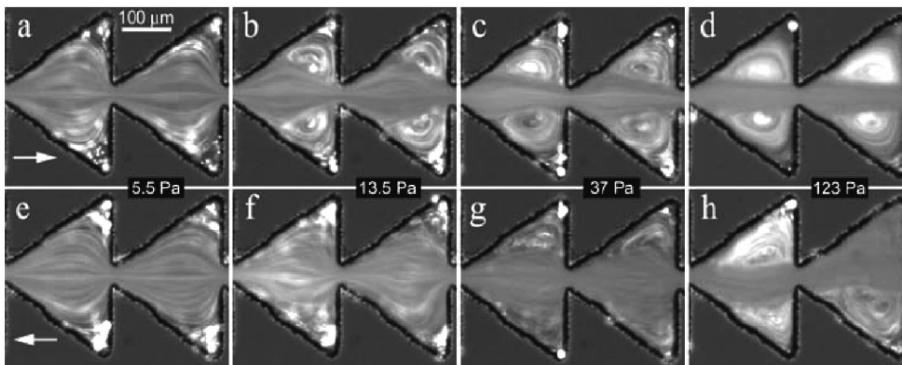
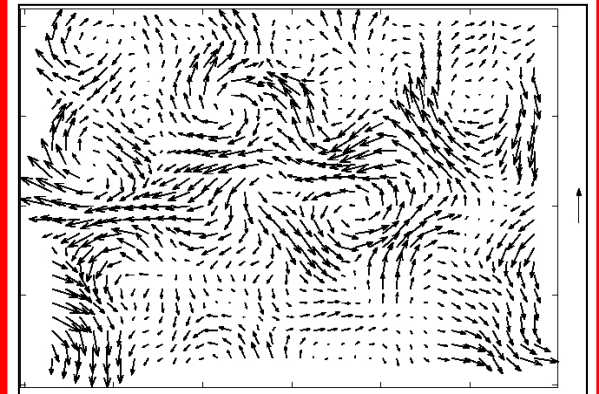
- Microfluidic rectifiers
- Groisman, Enzelberger, & Quake '03



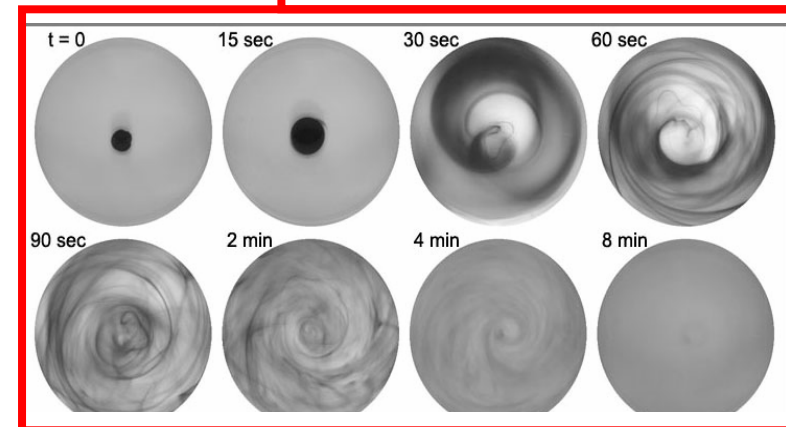
I-S_A phase trans -- PPM



B. subtilis – one and many
C. Dombrowski et al '05, '07



microfluidic rectifier – Groisman & Quake

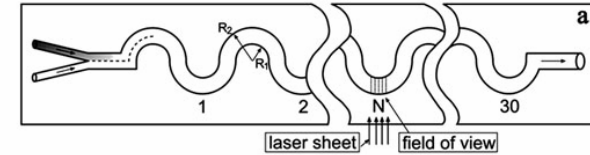
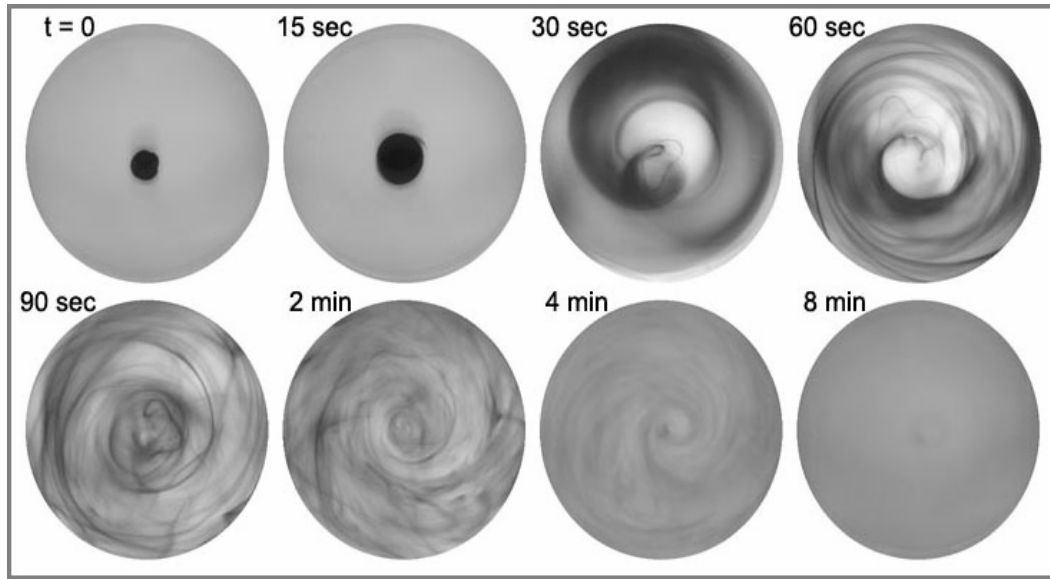


microscale mixing – Groisman & Steinberg

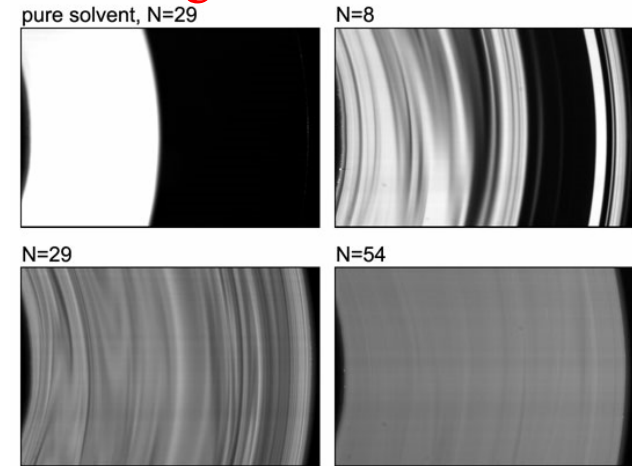
Experiments: V. Steinberg & A. Groisman

Viscoelastic fluid – Elastic “turbulence” - Efficient mixing

Rotating plates (Low Re, “High” Wi)

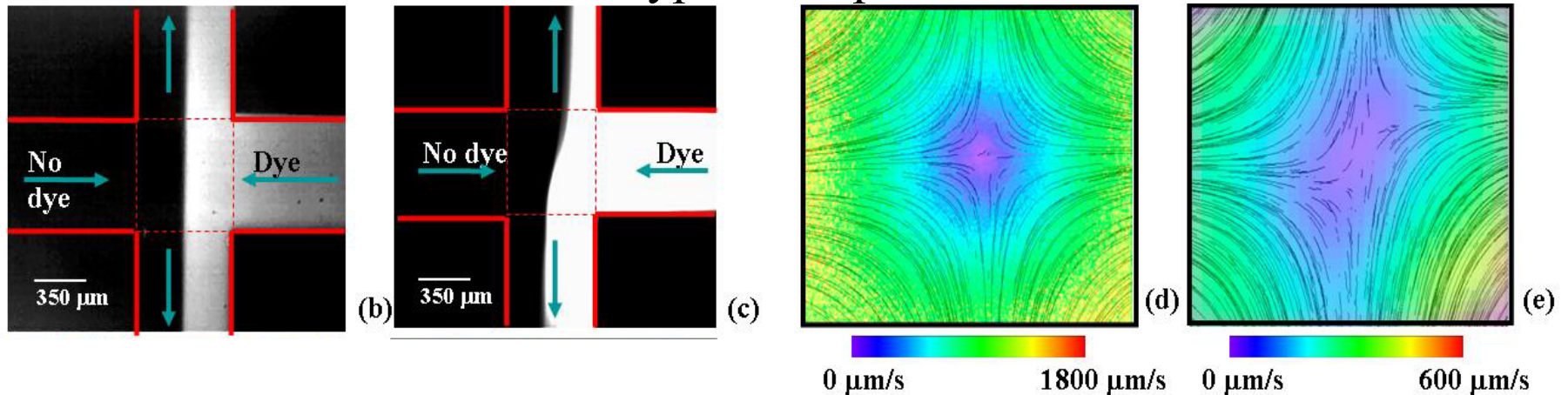


Mixing in micro channels



Arratia *et al*, PRL 2006

Elastic fluid instabilities near hyperbolic points



Stokes-Oldroyd-B ($Re \ll 1$)

- model of a “Boger” elastic fluid (normal stresses, no shear thinning)
- derives from a microscopic, dilute theory of polymer coils
- one of the standard viscoelastic flow models; Little known about large data solutions.

$$-\nabla p + \Delta \mathbf{u} = -\beta \nabla \cdot \boldsymbol{\sigma}_p - \mathbf{f} \quad \text{and} \quad \nabla \cdot \mathbf{u} = 0$$

momentum and mass balance

$$Wi \boldsymbol{\sigma}_p^\nabla = -(\boldsymbol{\sigma}_p - \mathbf{I})$$

transport and dissipation
of polymer stress

- $\boldsymbol{\sigma}_p^\nabla = \frac{D\boldsymbol{\sigma}_p}{Dt} - (\nabla \mathbf{u} \cdot \boldsymbol{\sigma}_p + \boldsymbol{\sigma}_p \cdot \nabla \mathbf{u}^T)$ Upper convected time derivative

- $Wi = \frac{\tau_p}{\tau_f}$; Weissenberg number ratio of polymer relax. time
to flow time-scale

$$\tau_f = \frac{\mu}{\rho L F}$$

- $\beta = \frac{G\tau_f}{\mu}$; coupling strength

μ = solvent viscosity; F = external force scale
 τ_p = polymer relaxation time; G = background poly. stress

- $\beta \cdot Wi = \frac{G\tau_p}{\mu} = \frac{\text{polymer viscosity}}{\text{solvent viscosity}}$

Material constant; fix to $\frac{1}{2}$
as in expts of Arratia *et al*

Properties:

(1) Has decaying "strain" energy: $E = \frac{1}{2} \int \text{tr}(\boldsymbol{\sigma}_p - \mathbf{I})$

$$\dot{E} + Wi^{-1}E = 2\beta^{-1} \left[-\int |\nabla \mathbf{u}|^2 + \int \mathbf{u} \cdot \mathbf{f} \right]$$

(2) But lacks of scale dependent dissipation:

$$\frac{\partial \hat{\boldsymbol{\sigma}}_p}{\partial t} = L(\hat{\mathbf{k}}) \hat{\boldsymbol{\sigma}}_p + P(\hat{\mathbf{k}}) \hat{\mathbf{f}}$$

$$\text{with } \hat{\mathbf{k}} = \mathbf{k} / |\mathbf{k}|$$

Use the Fourier transform
to solve the linearized
problem

(3) Polymer stress tensor: $\boldsymbol{\sigma}_p = \nu \langle \mathbf{fr} \rangle = C \langle \mathbf{rr} \rangle$ ← Assume linear Hooke's law for bead forces

is s.p.d.

(4) Existence of large-data solutions is unknown, even in 2d

Simulations: De-aliased Fourier based spectral method;
second order time stepping.

Vorticity field for Newtonian fluid

Background force

$$\mathbf{f} = \begin{pmatrix} -2 \sin x \cos y \\ 2 \cos x \sin y \end{pmatrix}$$

With Newtonian fluid
yields

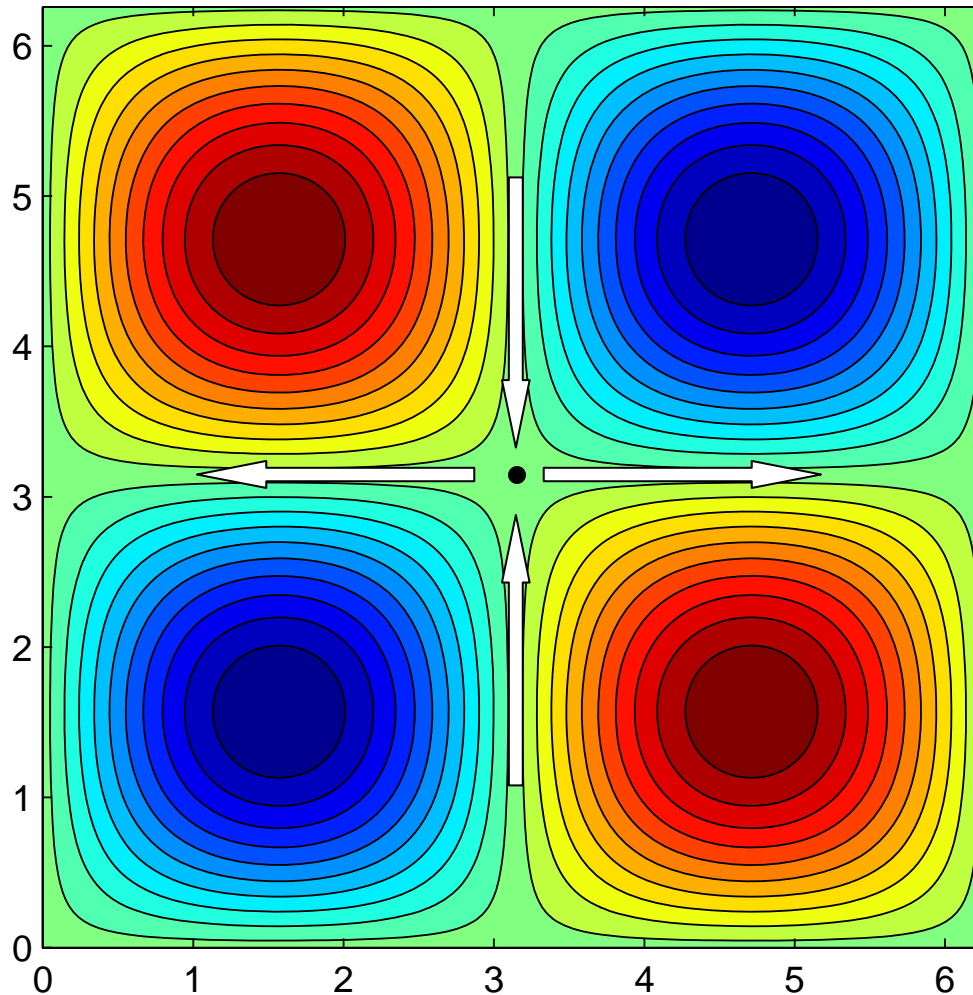
$$\mathbf{u} = \begin{pmatrix} \sin x \cos y \\ -\cos x \sin y \end{pmatrix}$$

Creates hyperbolic points
in background flow

ala Arratia et al., PRL 2006

Also Berti et al '08, Xi & Graham '09
Becherer, Morozov, van Saarloos '08, 09

Four – roll mill geometry

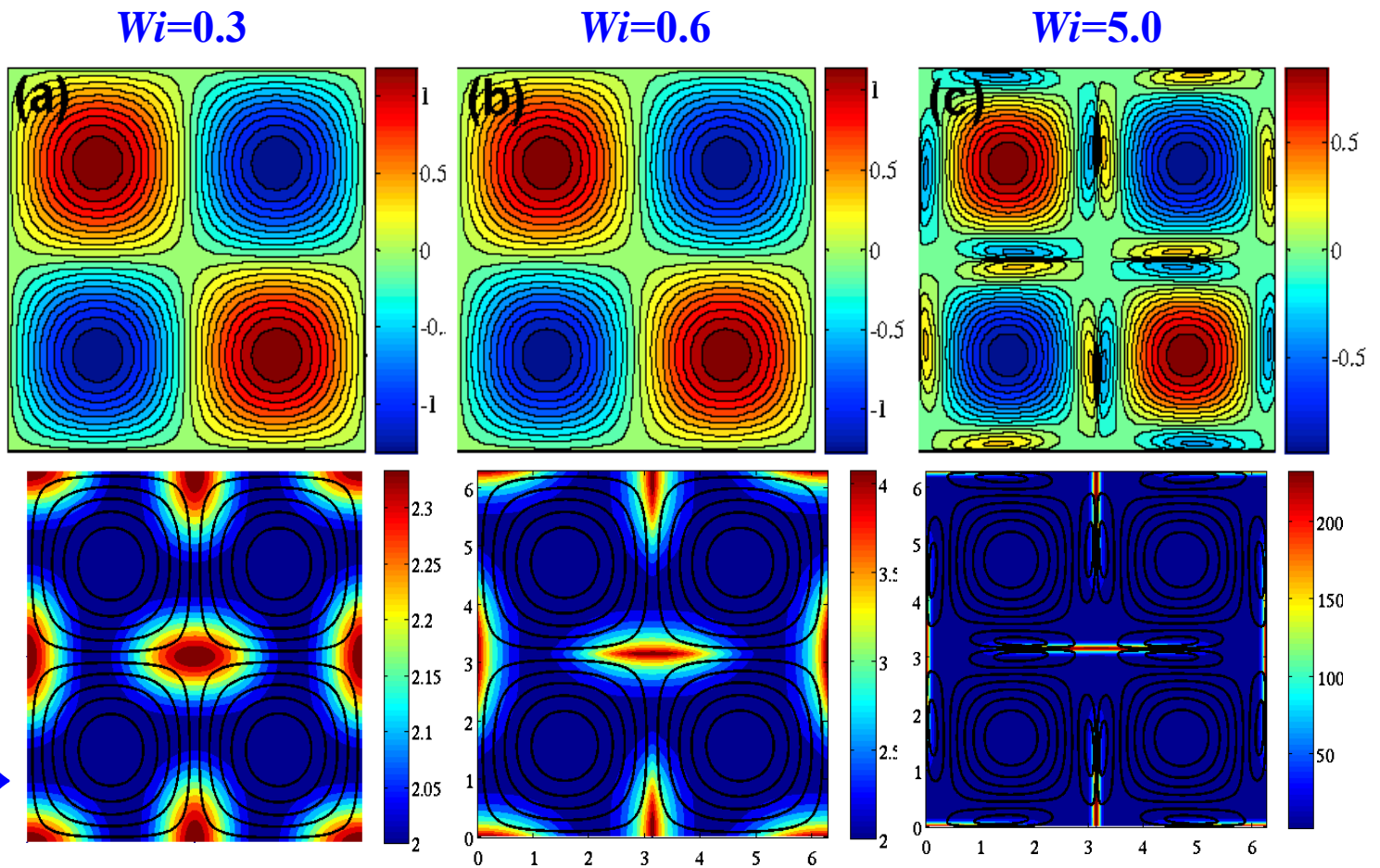


Thomases & Shelley *PF* 2007

Evolution for
initial stress:

$$\boldsymbol{\sigma}_p(t=0) = \mathbf{I}$$

$\omega \rightarrow$

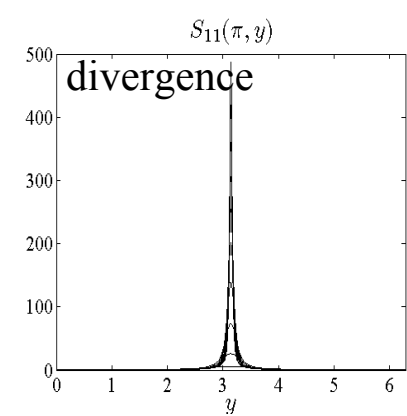
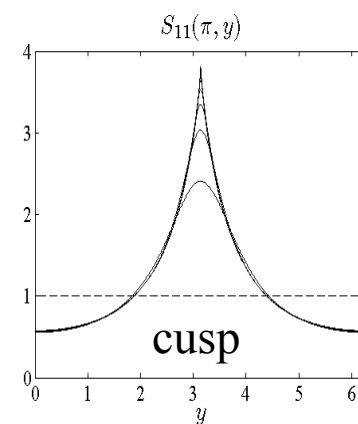
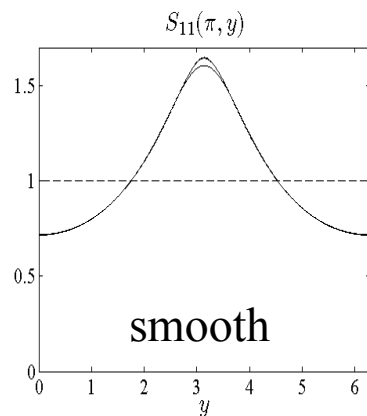


$\text{tr}(\boldsymbol{\sigma}_p) \rightarrow$

slices of

$$\boldsymbol{\sigma}_p^{11}$$

\rightarrow



Local Model – fix strain-rate α – determined by flow -- and advect stress field by local straining velocity

$$\tilde{u} = (\alpha x, -\alpha y); \quad \varphi = \sigma_p^{11}; \quad t \rightarrow Wi \cdot t; \quad \varepsilon = \alpha \cdot Wi$$

$$\varphi_t + \varepsilon x \varphi_x - \varepsilon y \varphi_y + (1 - 2\varepsilon)\varphi - 1 = 0$$

General solution :

$$\varphi = \frac{1}{1-2\varepsilon} + e^{(2\varepsilon-1)t} H_{11}(xe^{-\varepsilon t}, ye^{\varepsilon t})$$

Relevant solution : $H_{11}(a, b) = h(b)$ with $h(b) \sim |b|^q$ as $|b| \rightarrow \infty$

Why? Choose q to eliminate long time t – dependence

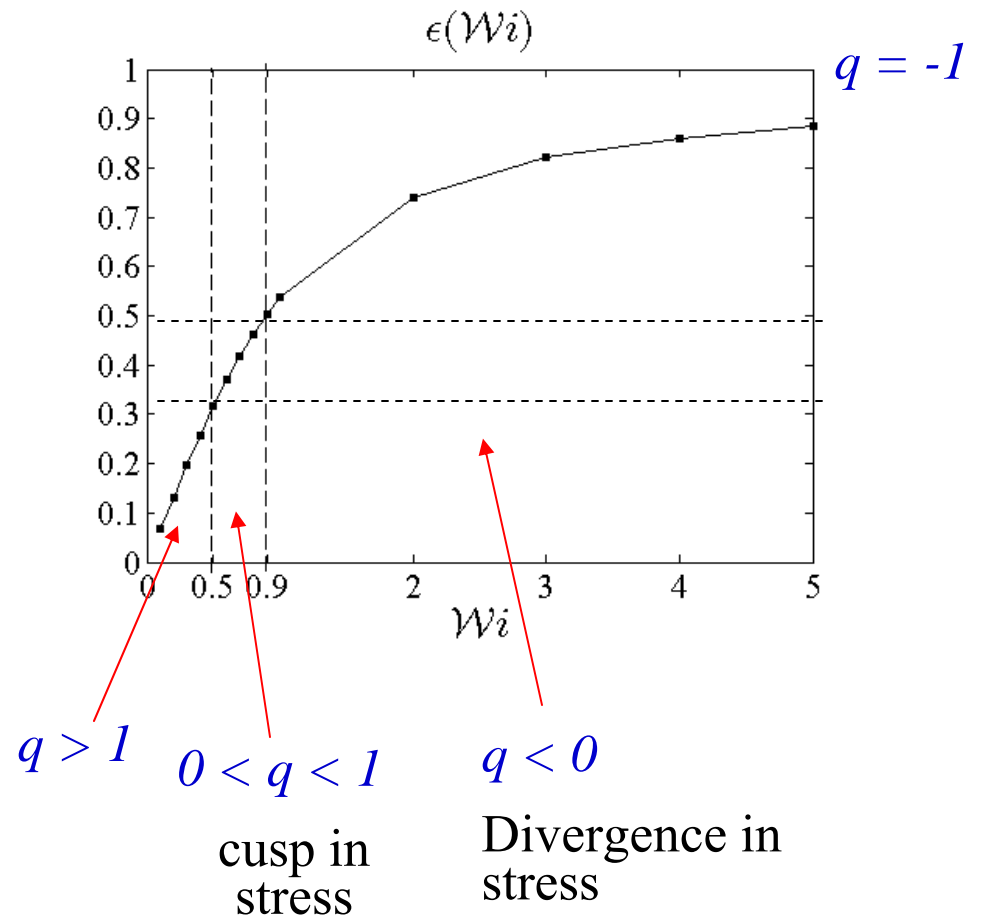
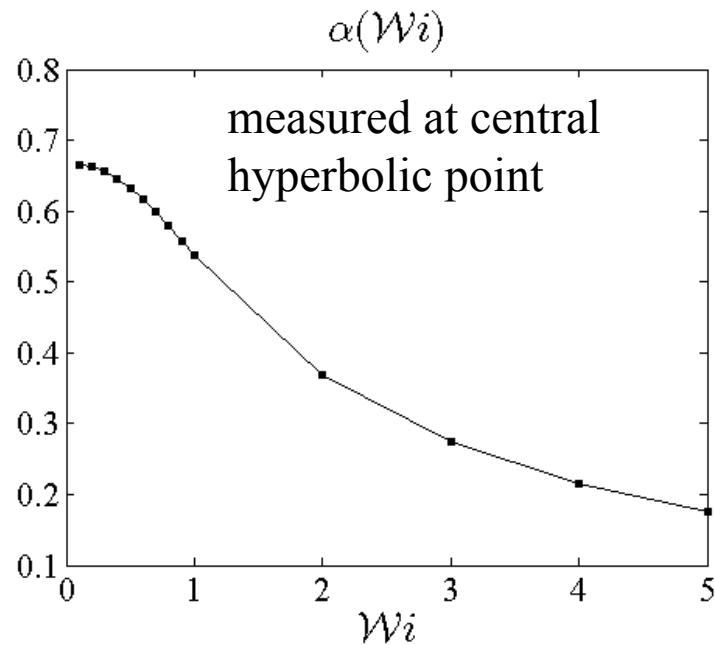
$$\Rightarrow q = \frac{1-2\varepsilon}{\varepsilon} \Rightarrow \varphi|_{t \rightarrow \infty} = \frac{1}{1-2\varepsilon} + C |y|^{\frac{1-2\varepsilon}{\varepsilon}}$$

steady states also studied by Rallison & Hinch '88 and M. Renardy '06

$$\varepsilon = \alpha(Wi)Wi; \quad q = \frac{1-2\varepsilon}{\varepsilon}$$

$$\varepsilon_1 = 1/3 \quad Wi_1 \approx 0.5$$

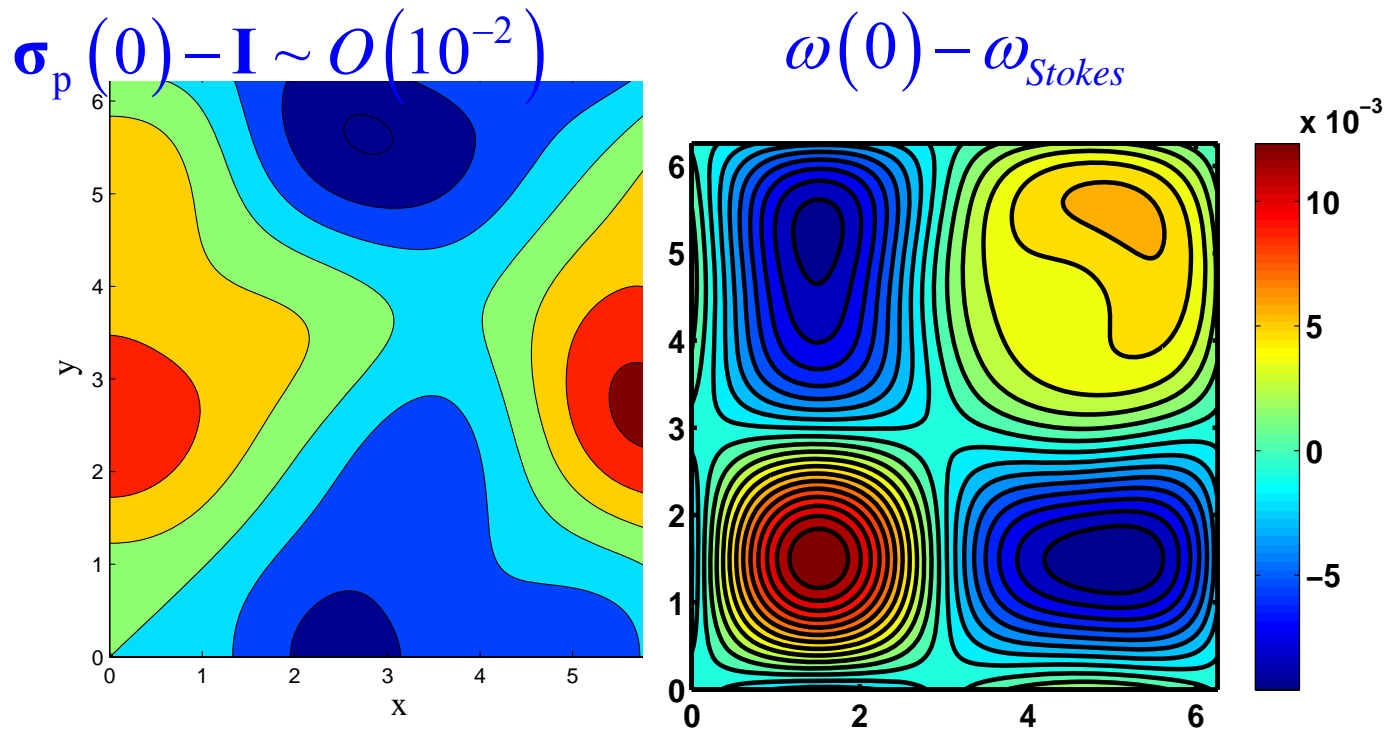
$$\varepsilon_2 = 1/2 \quad Wi_2 \approx 0.9$$



Note $\varepsilon < 1$ implies $q > -1$ so the stress is integrable.

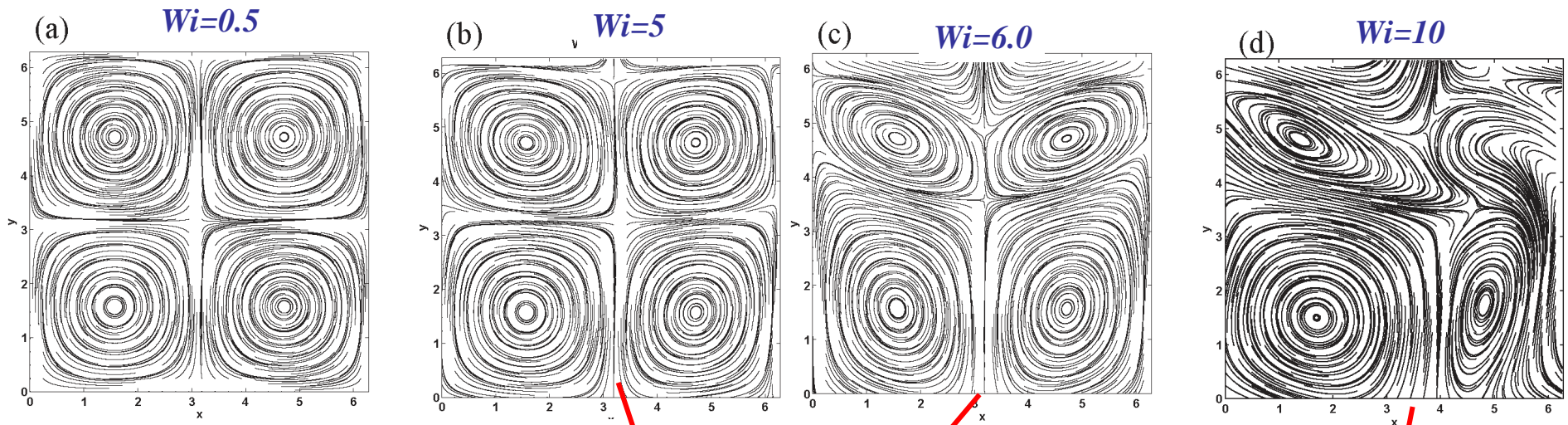
Mixing and Symmetry-Breaking: Thomases & Shelley '09

The SOB system is also unstable to symmetry-breaking;
see Poole *et al* '07, Xi & Graham '08



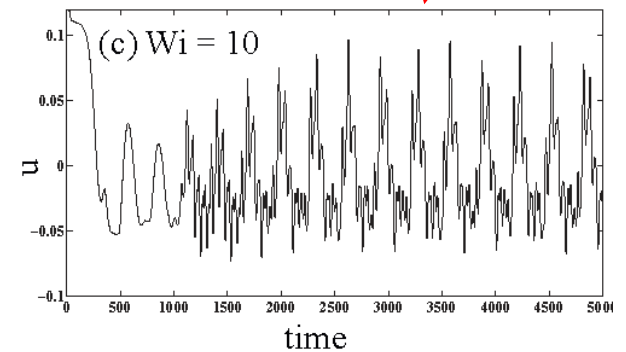
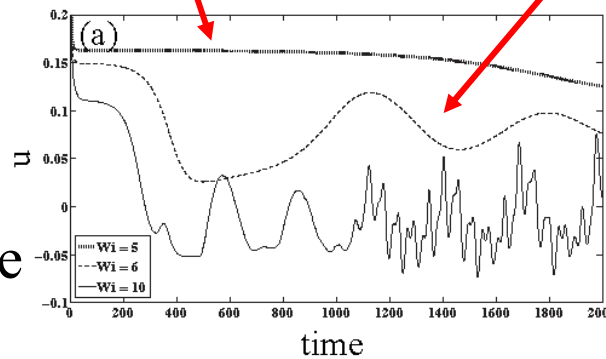
Full disclosure: Small amount of polymer stress diffusion added to control gradient growth

Long-time behavior with increasing Wi :

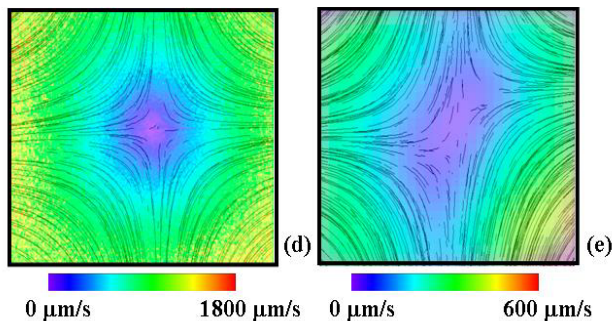


relaxation to symmetric state

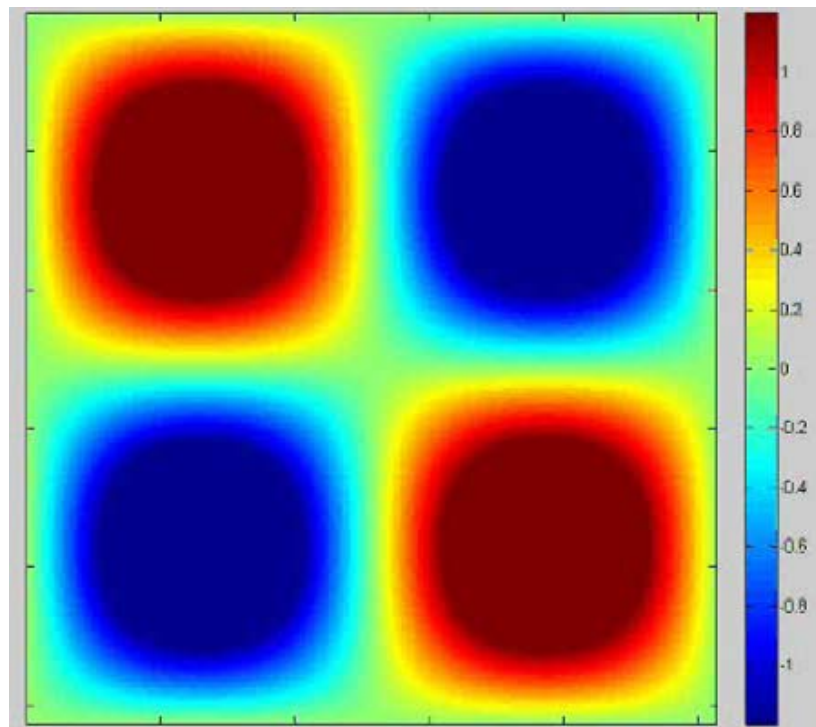
Slow relaxation to asymmetric state



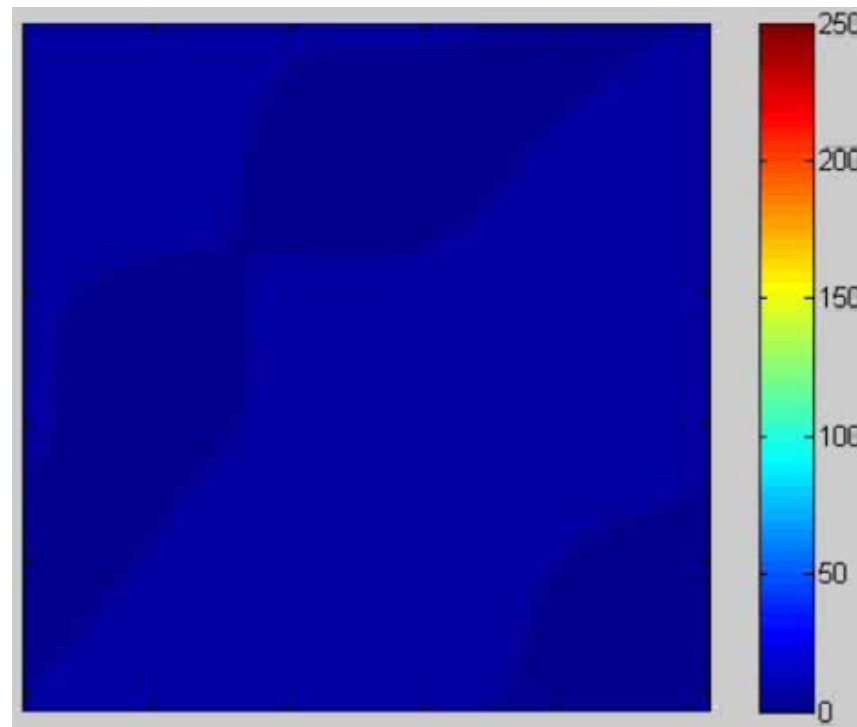
Persistent oscillations



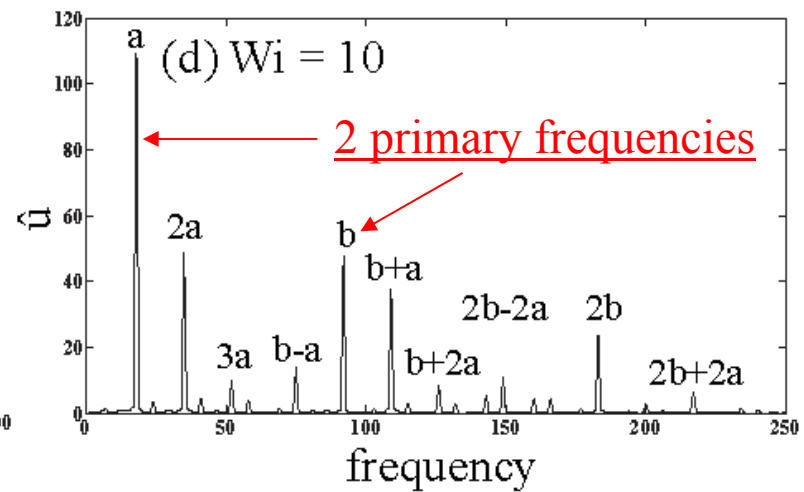
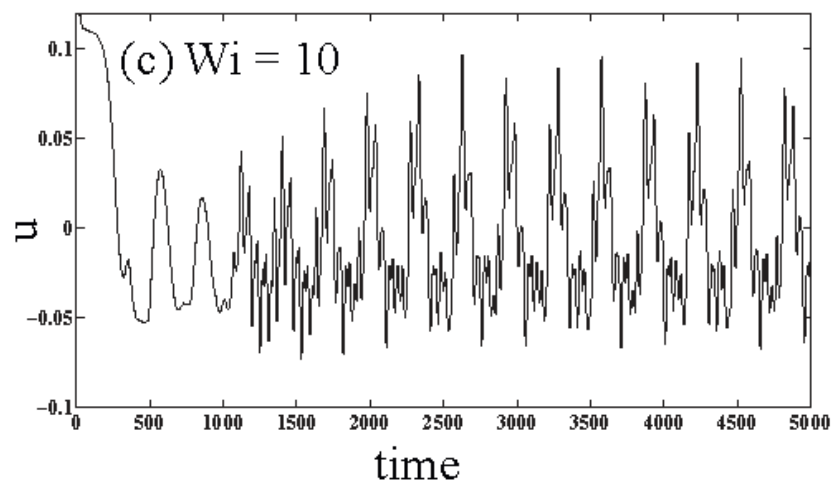
Arratia et al '06



ω



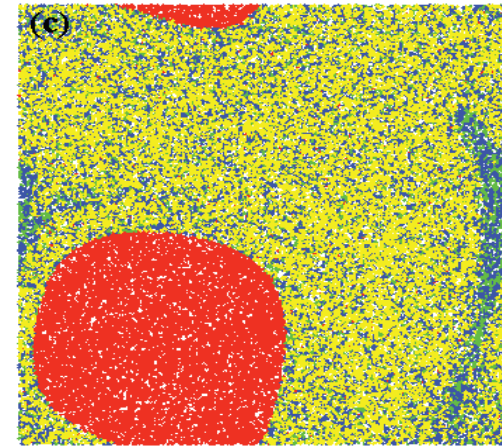
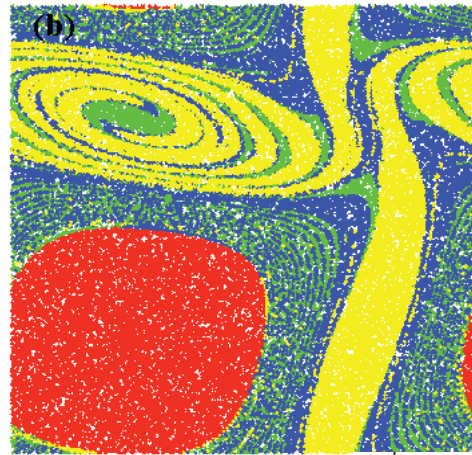
$\text{tr}(\sigma_p)$





$Wi=6, t=2000$

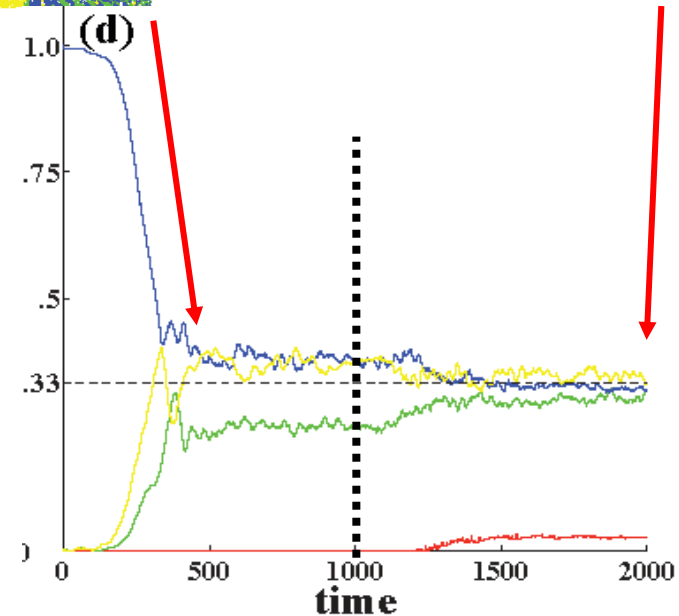
Smaller Wi :
symmetry breaking, little mixing



Larger Wi :

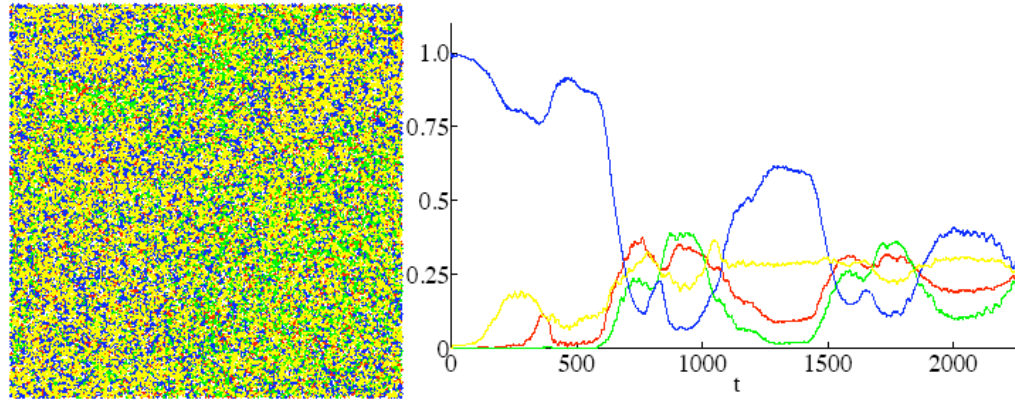
- multiple frequencies of oscillation
- robust GRS of viscoelastic flows
- well-mixed fluid outside of GRS

Need new experiments,
stability analyses.



Update:

- (1) 1 of 10 simulations using random amplitude/phase initial perturbations for polymer stress.

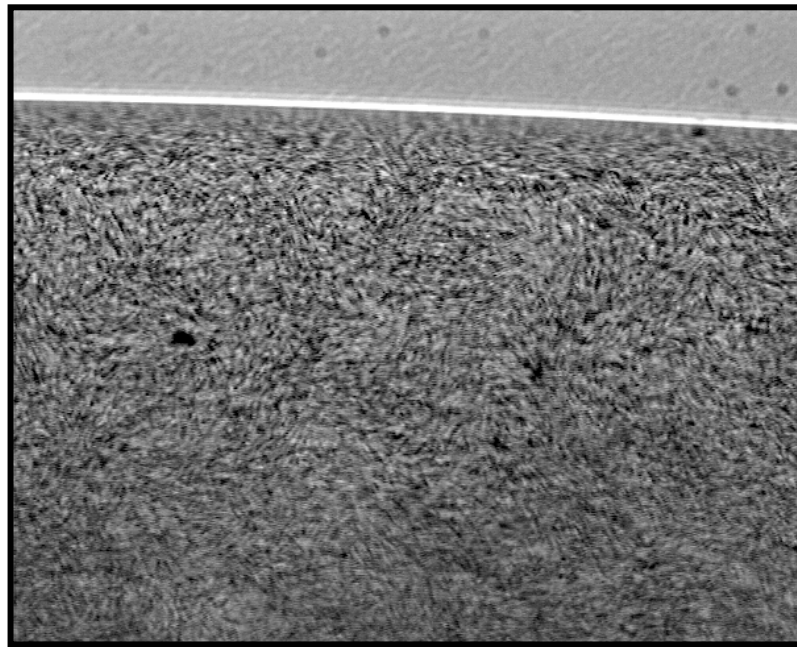


- (2) What if the number of vortex cells is increased?
- (3) Now investigating in a new expt'l rig in the AML



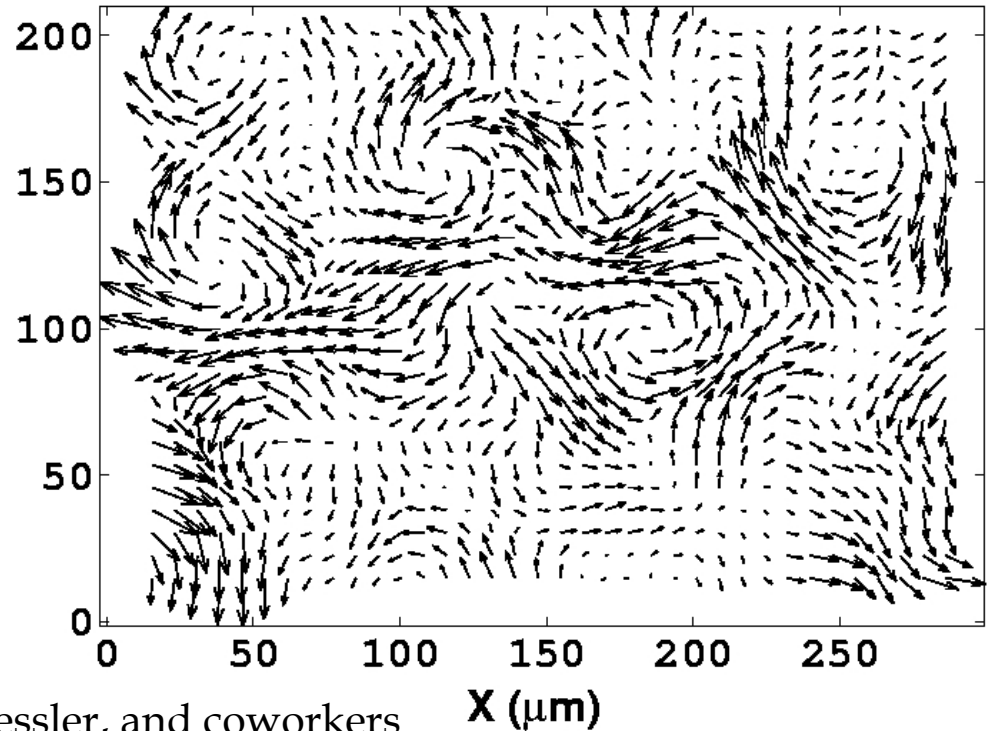
16 counter-rotating rotors driving a PAA viscoelastic solution
w. Bin Liu, J. Zhang

Collective dynamics of active suspensions (bacterial baths)



150 μm

R. Goldstein, J. Kessler, and coworkers



Observation: meandering jet and vortices of scale 50-100 μm , speeds 50-100 $\mu\text{m}/\text{sec}$ in jets
Scale of *B. subtilis* $\sim 4 \mu\text{m}$ (plus tail); swimming speed 20-30 $\mu\text{m}/\text{sec}$

-
- A complex fluid driven by dynamics of its microstructure – many body interactions mediated by fluid.
 - collective behavior leads to strong mixing.
 - Role of body geometry? Emergence or role of orientational ordering?
 - Competition of hydrodynamic coupling vs. attractive gradients?

Some of the experiments:

- Wu & Libchaber '00: “brownian” motion of test particles in bacterial baths.
- Dombrowski *et al* '04: large-scale flow structures (many body lengths).
- Kim & Breuer '04, enhanced mixing using bacteria in micro-fluidic device.
- Paxton *et al*, '04, fabricated chemically-driven nano-rod-swimmers.
- Dreyfus *et al*, '05, bio-mimetic swimmers driven by magnetic fields
- Short *et al*, '06, expts and model of *Volvox* swimming.
- Sokolov *et al*, '07, expts on concentration dependencies in thin films.
- ...

Some of the theory:

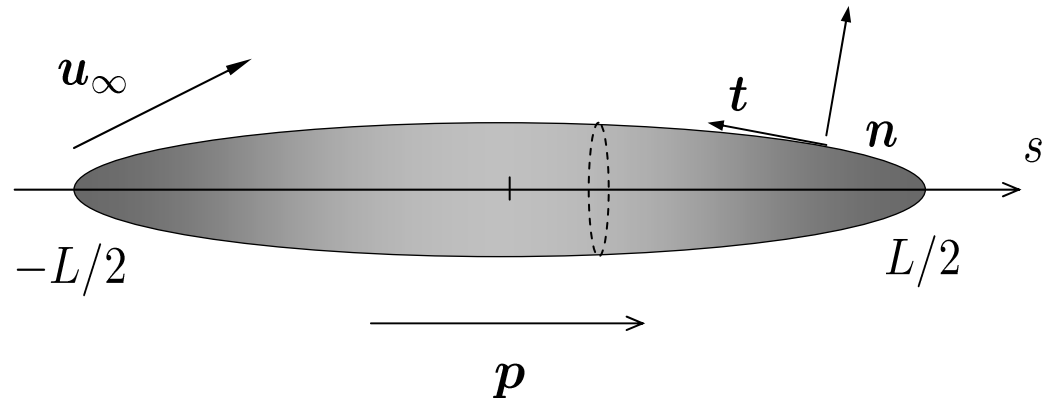
- bioconvection: Childress & Spiegel, Pedley and many others
- Simha & Ramaswamy '02: predict instability of long-wave oriented states
- Hernandez-Ortiz *et al*, '05: simulations of force-dipole suspensions show emergence of large-scale structures
- Toner *et al*, '05: models of flocking.
- Sabelashvili, Lau, & Cai '07, ordering of 2d rod locomotors by local steric interactions
- Pedley, Ishikawa *et al*, interactions of *squirmers* (specified surface velocity)
- Saintillan & Shelley, '07, '08, particle simulations, kinetic theory of moving rod suspensions
- Keaveny & Maxey, '08, theory and simulations for bio-mimetic swimmers
- Kanevsky *et al*, '09, simulations of interacting stress-actuated swimmers
- ...

Slender-body swimmer driven by surface stress

Saintillan & Shelley *PRL* 2007 , motivated by Volvox model of Short, Goldstein, *et al*;
 (simulation of multi-V interactions by Kanevsky, Shelley, Tornberg, '08)

Surface tractions:

$$\boldsymbol{\sigma}(s, \theta) \cdot \mathbf{n} = \underbrace{f_0(s)}_{\text{prescribed}} \mathbf{t} + \underbrace{g(s, \theta)}_{\text{unknown}} \mathbf{n}$$



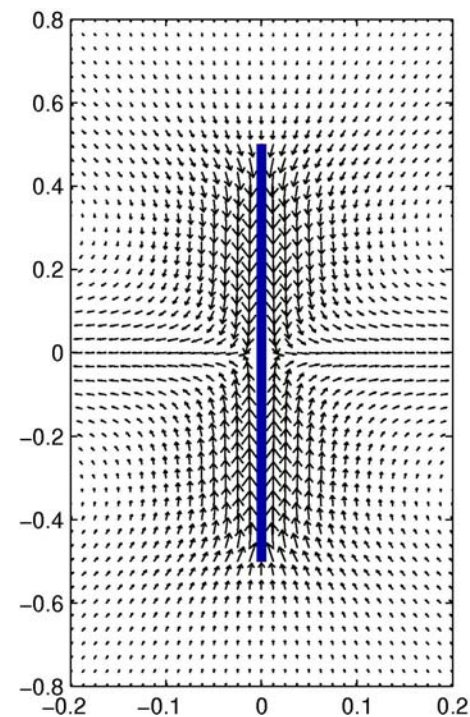
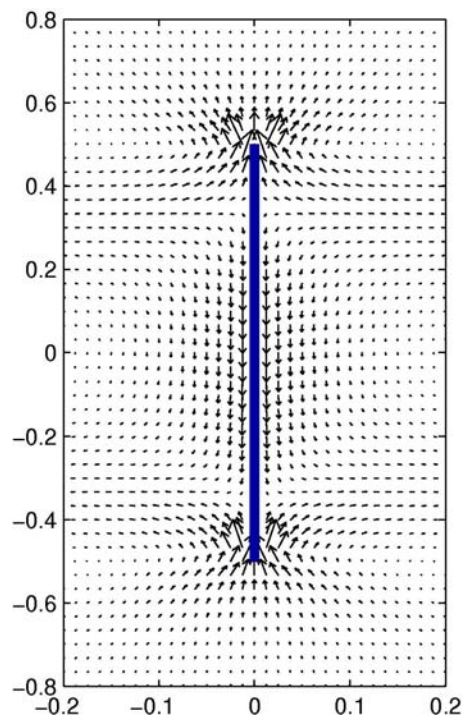
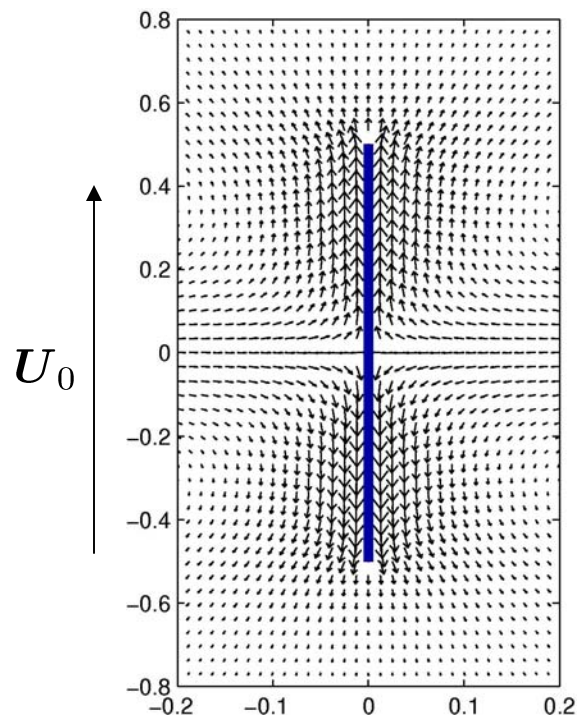
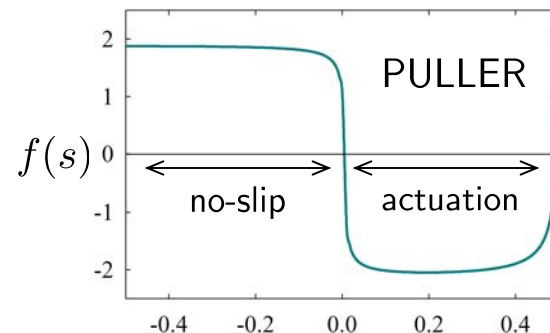
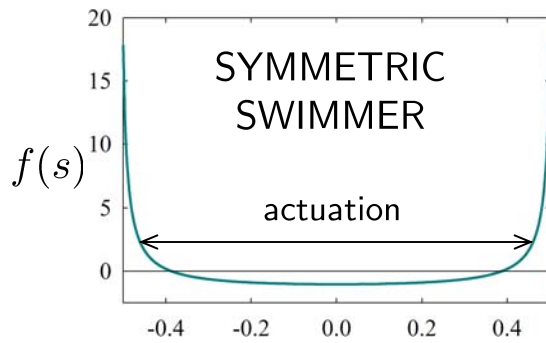
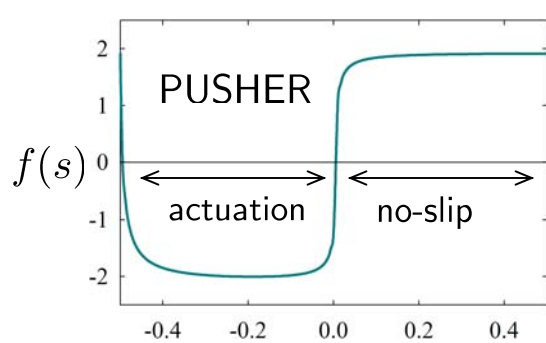
Integrated traction (force per unit length):

$$\mathbf{f}(s) = \int_0^{2\pi} \boldsymbol{\sigma}(s, \theta) \cdot \mathbf{n} r(s) d\theta = \underbrace{2\pi f_0(s) r(s) m(s)}_{\substack{\mathbf{f}_{\parallel}, \text{ prescribed} \\ (m(s) = \mathbf{t}(s) \cdot \mathbf{p})}} \mathbf{p} + \underbrace{\mathbf{f}_{\perp}(s)}_{\text{unknown}}$$

Force and torque balances:

$$\mathbf{F} = \int_{-L/2}^{L/2} \mathbf{f}(s) ds = \mathbf{0}, \quad \mathbf{T} = \int_{-L/2}^{L/2} s \mathbf{p} \times \mathbf{f}(s) ds = \mathbf{0}$$

Single particle flow fields



FAR FIELD: $|\mathbf{u}(\mathbf{x})| \sim U_0 \left(\frac{L}{|\mathbf{x}|}\right)^2$
(stresslet)

$|\mathbf{u}(\mathbf{x})| \sim U_0 \left(\frac{L}{|\mathbf{x}|}\right)^3$
(Stokes quadrupole)

$|\mathbf{u}(\mathbf{x})| \sim U_0 \left(\frac{L}{|\mathbf{x}|}\right)^2$
(stresslet)

Saintillan & Shelley, *PRL* '07

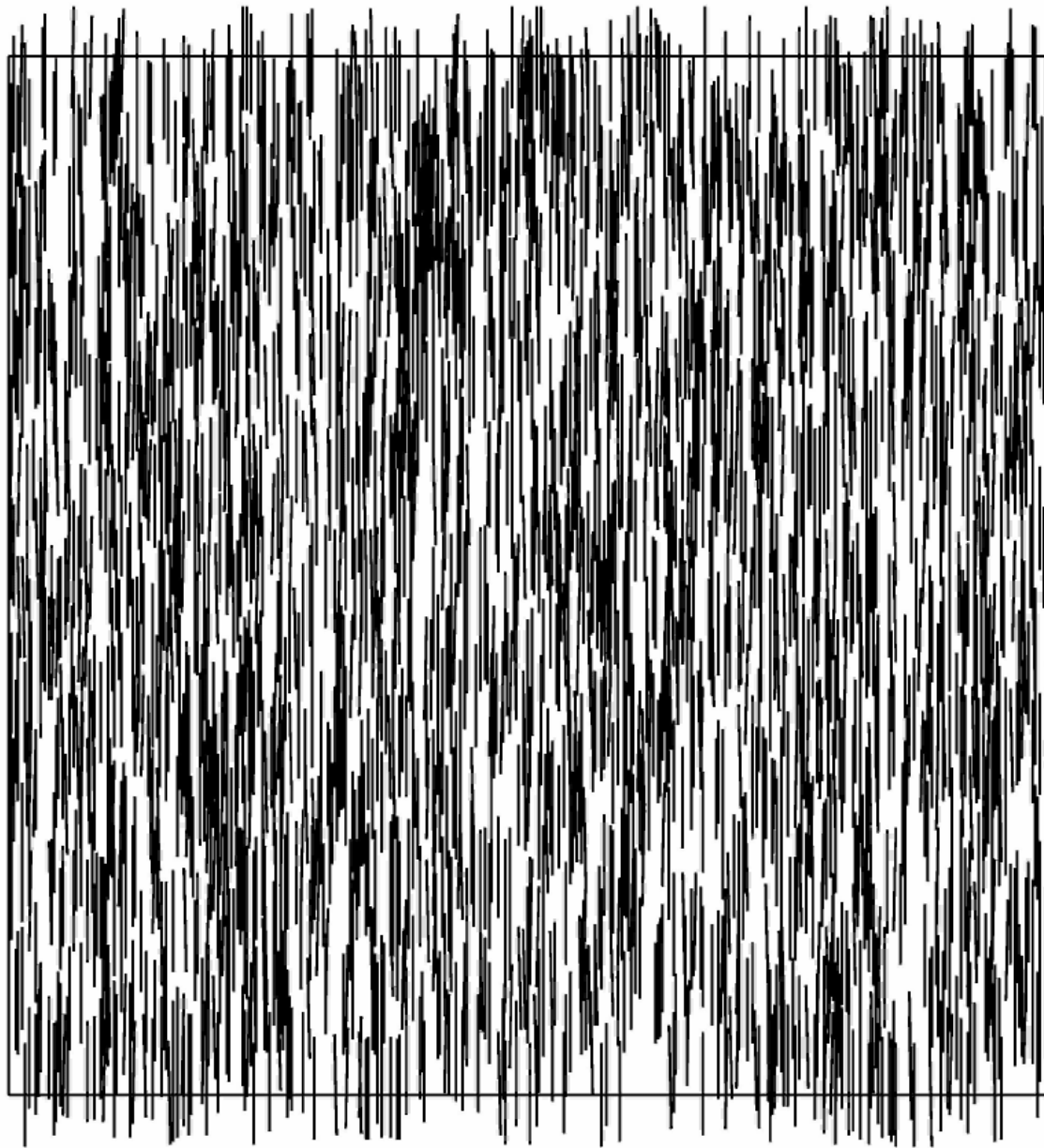
2500 swimming “pushers” in
periodic box of dimensions

10 x 10 x 3

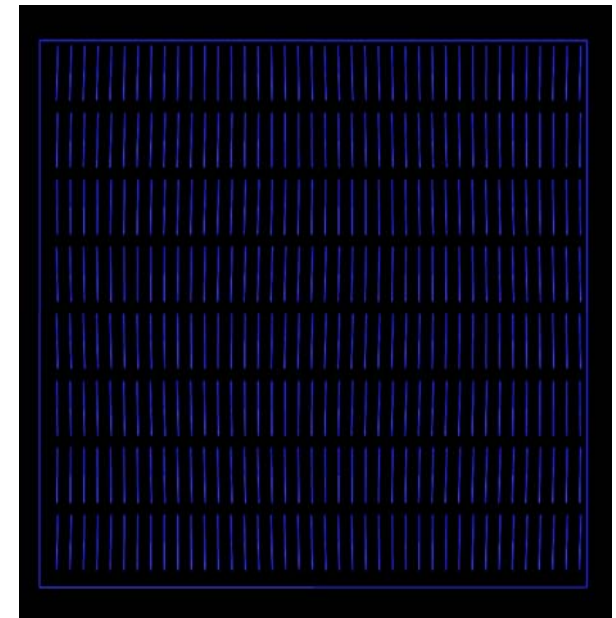
effective volume fraction

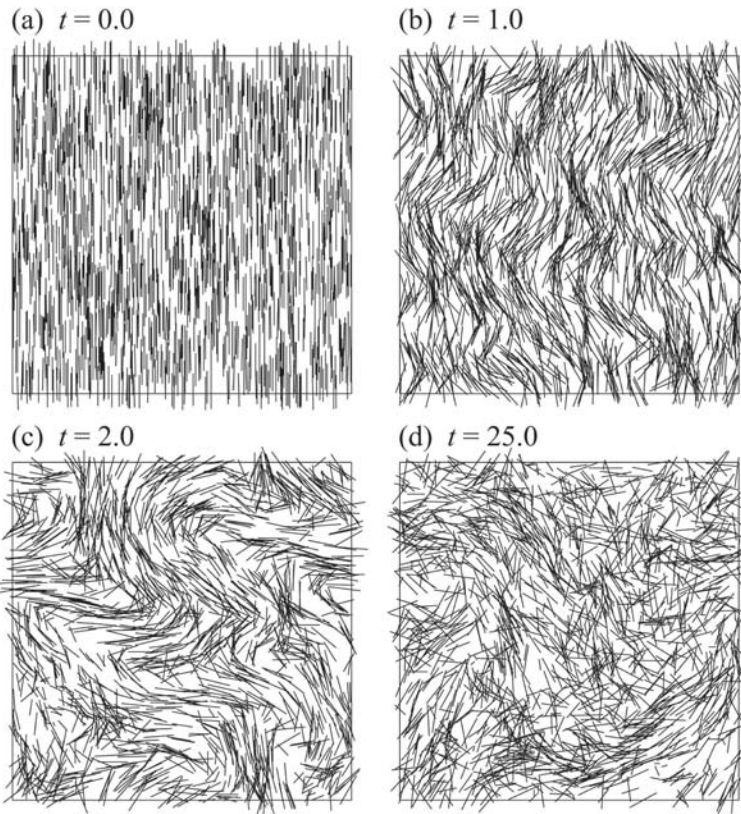
$n (L/2)^3 = 1$; $n = \#$ density
(strongly interacting)

All initially aligned in the
 \mathbf{z} direction – nematic order –
with randomized positions

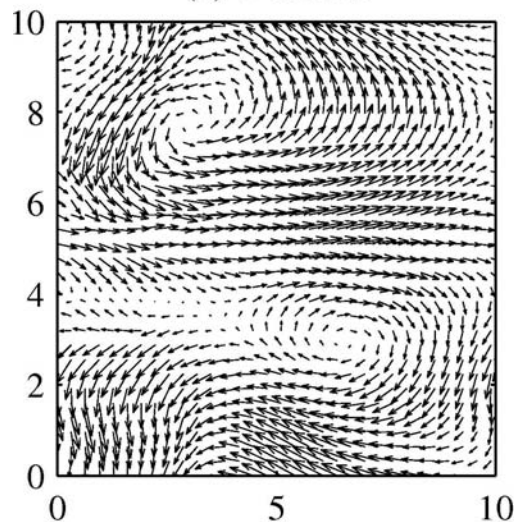


← 10 →

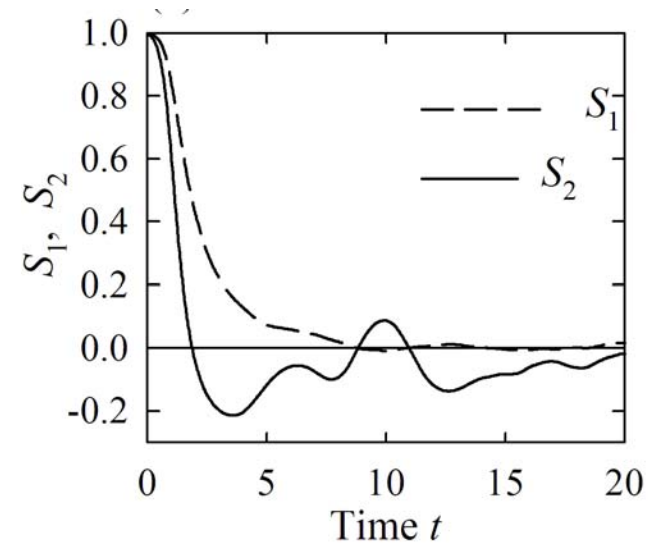




(a) Pushers



Spatially organized instability destroys long-range order. Predicted by Simha & Ramaswamy '02



Loss of global orientational order:
order parameters:

$$S_1 = \langle \mathbf{p} \cdot \mathbf{z} \rangle \quad \& \quad S_2 = \frac{1}{2} \left(3 \langle \mathbf{p} \cdot \mathbf{z} \rangle^2 - 1 \right)$$

Emergence of large-scale dynamical flow
as in *Dombrowski et al*, *Hernandez-Ortiz et al*

A kinetic theory for active suspensions S&S, PRL '08, PF '08

Pose Fokker-Planck equation for distribution function $\Psi(\mathbf{x}, \mathbf{p}, t)$ of particle center of mass \mathbf{x} and (unit) swimming director \mathbf{p} (rod theory, Doi & Edwards, '86) :

$$\Psi_t + \nabla_x \cdot (\dot{\mathbf{x}}\Psi) + \nabla_p \cdot (\dot{\mathbf{p}}\Psi) = 0 \quad \text{with} \quad \frac{1}{V} \int dV_x \int dS_p \Psi = n$$

w. "particle" fluxes $\left\{ \begin{array}{l} \dot{\mathbf{x}} = \underline{U_0} \mathbf{p} + \mathbf{u}(\mathbf{x}, t) - \nabla_x (D \ln \Psi) \\ \dot{\mathbf{p}} = (\mathbf{I} - \mathbf{p}\mathbf{p})(\gamma \mathbf{E} + \mathbf{W})\mathbf{p} - \nabla_p (d \ln \Psi) \end{array} \right.$

Background fluid velocity:

$$\nabla q - \Delta \mathbf{u} = \nabla \cdot \boldsymbol{\Sigma}^a \quad \text{and} \quad \nabla \cdot \mathbf{u} = 0$$

driven by active swimming stress (Kirkwood theory; Batchelor '70):

$$\boldsymbol{\Sigma}^a(\mathbf{x}, t) = \underline{\sigma_0} \int dS_p \Psi(\mathbf{x}, \mathbf{p}, t) [\mathbf{p}\mathbf{p} - \mathbf{I}/3]$$

Pushers: $\sigma_0 < 0$; Pullers: $\sigma_0 > 0$

Important d'less parameters: $U_0 \rightarrow 1$, $\sigma_0 \rightarrow \alpha = O(1)$, $L \rightarrow L/l_c$

A useful special case

Neglecting diffusion, consider a locally aligned suspension:

$$\Psi(\mathbf{x}, \mathbf{p}, t) = c(\mathbf{x}, t) \delta(\mathbf{p} - \mathbf{n}(\mathbf{x}, t))$$

Setting $D=d=0$ The full kinetic equations reduce exactly to:

$$\left\{ \begin{array}{l} \frac{\partial c}{\partial t} + \nabla_x \cdot ((\mathbf{n} + \mathbf{u})c) = 0 \\ \frac{\partial \mathbf{n}}{\partial t} + (\mathbf{n} + \mathbf{u}) \cdot \nabla_x \mathbf{n} = (\mathbf{I} - \mathbf{nn}) \nabla_x \mathbf{u} \mathbf{n} \quad (\text{preserves } \mathbf{n} \cdot \mathbf{n} = 1) \end{array} \right.$$

with $\nabla_x q - \nabla_x^2 \mathbf{u} = -\nabla_x \cdot \Sigma^a, \quad \nabla_x \cdot \mathbf{u} = 0$

and particle
extra stress

$$\Sigma^p = \alpha c(\mathbf{x}, t)(\mathbf{nn} - \mathbf{I}/3)$$

Stability analysis II: uniform isotropic case

A nearly isotropic uniform suspension:

$$\Psi(\mathbf{x}, \mathbf{p}, t) = \frac{1}{4\pi} \left[1 + \varepsilon \tilde{\Psi}_{\mathbf{k}}(\mathbf{p}) e^{i(\mathbf{k} \cdot \mathbf{x} + \lambda t)} \right]$$

Derive relation:

$$\tilde{\Psi}_{\mathbf{k}} = -\frac{3i\alpha\gamma}{2\pi} \frac{\hat{\mathbf{k}} \cdot \mathbf{p}}{\lambda + i\mathbf{k} \cdot \mathbf{p} + Dk^2} \mathbf{p} \cdot \mathbf{F}[\tilde{\Psi}_{\mathbf{k}}] \quad (1)$$

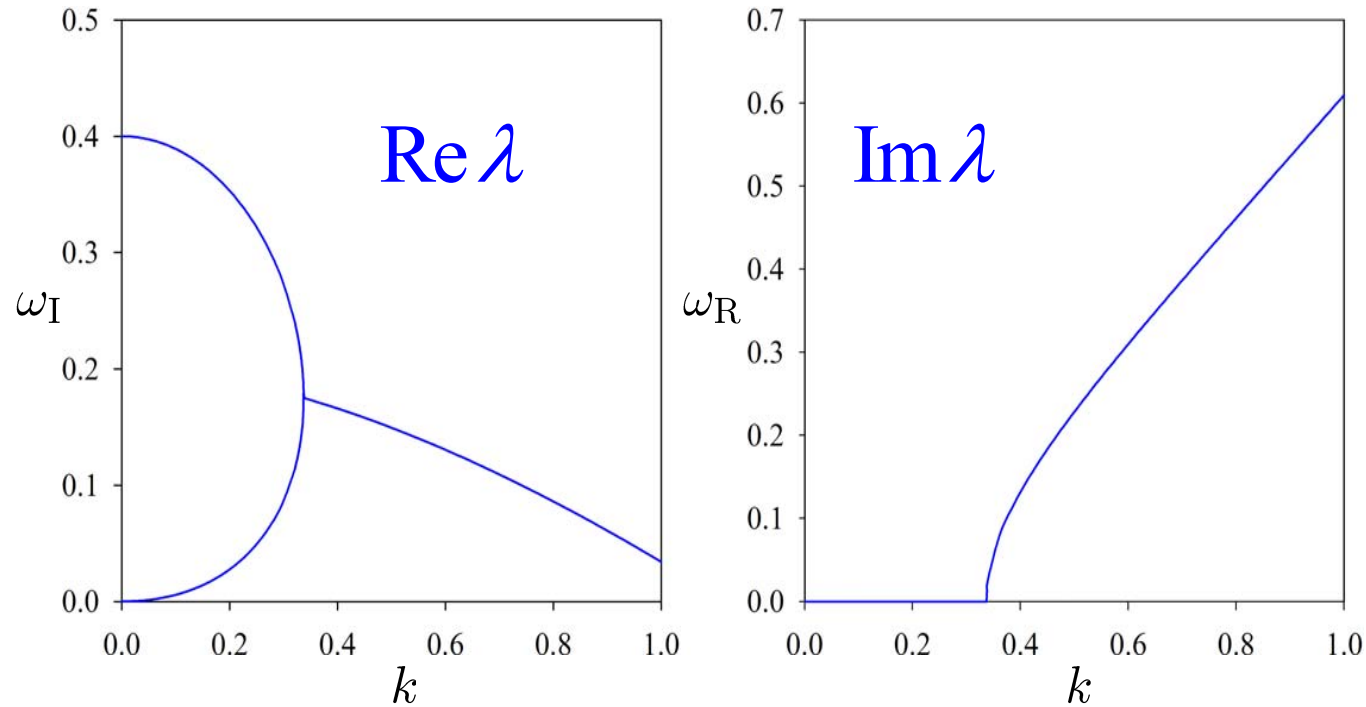
where

$$\mathbf{F}[\tilde{\Psi}_{\mathbf{k}}] = (\mathbf{I} - \hat{\mathbf{k}}\hat{\mathbf{k}}) \int dS_{p'} \mathbf{p}' (\hat{\mathbf{k}} \cdot \mathbf{p}') \tilde{\Psi}_{\mathbf{k}}(\mathbf{p}')$$

Applying \mathbf{F} operator to (1), and evaluation of the integral, yields the eigenvalue relation:

$$\frac{3i\alpha\gamma}{2k} \left[2a^3 - \frac{4}{3}a + (a^4 - a^2) \log \frac{a-1}{a+1} \right] = 1 \quad \text{w. } a = -i(\lambda + Dk^2)/k$$

$\alpha = -1$ (pushers), $\gamma = 1$ (rods), $D = 0$



Suspensions of *pushers* are *unstable* at long wavelengths.
pullers are stable

(eigen-solutions do not describe small-scale behavior – [Hohenegger & Shelley '09](#))

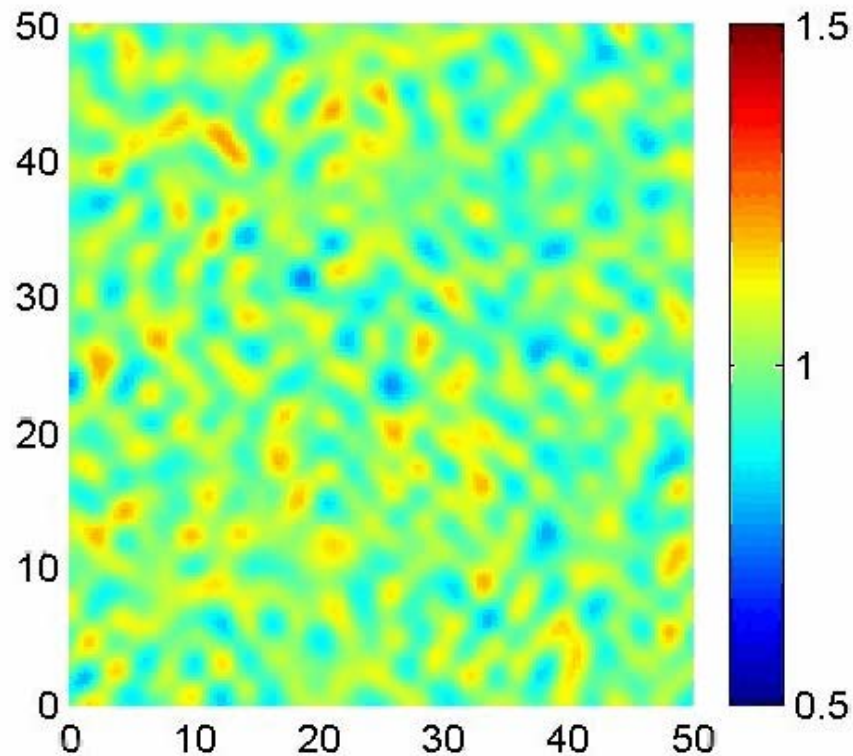
Eigenfunctions: $\tilde{c}_{\mathbf{k}} = \int dS_p \tilde{\Psi}_{\mathbf{k}}(\mathbf{p}) = 0$ no concentration fluctuations in linear theory.

$\tilde{\Sigma}_{\mathbf{k}}^a = \mathbf{k}\mathbf{k}_{\perp} + \mathbf{k}_{\perp}\mathbf{k}$ active stress eigen-modes are shear-stresses.

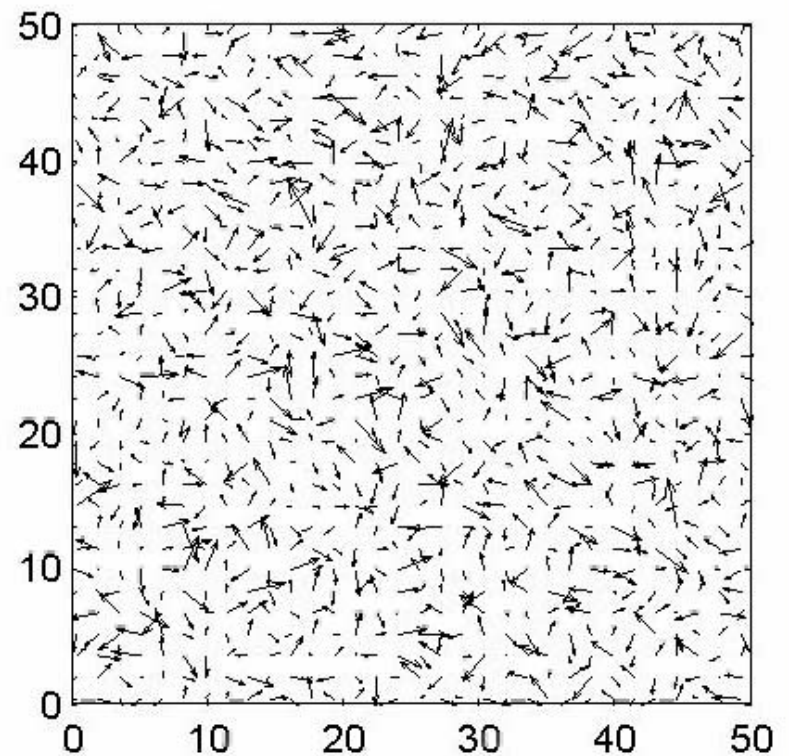
Non-linear simulations (2-d)

▪ **Initial condition:**
$$\Psi(\mathbf{x}, \phi, 0) = \frac{1}{2\pi} \left[1 + \sum_i \epsilon_i \cos(\mathbf{k}_i \cdot \mathbf{x} + \xi_i) \times P_i(\cos \phi, \sin \phi) \right]$$

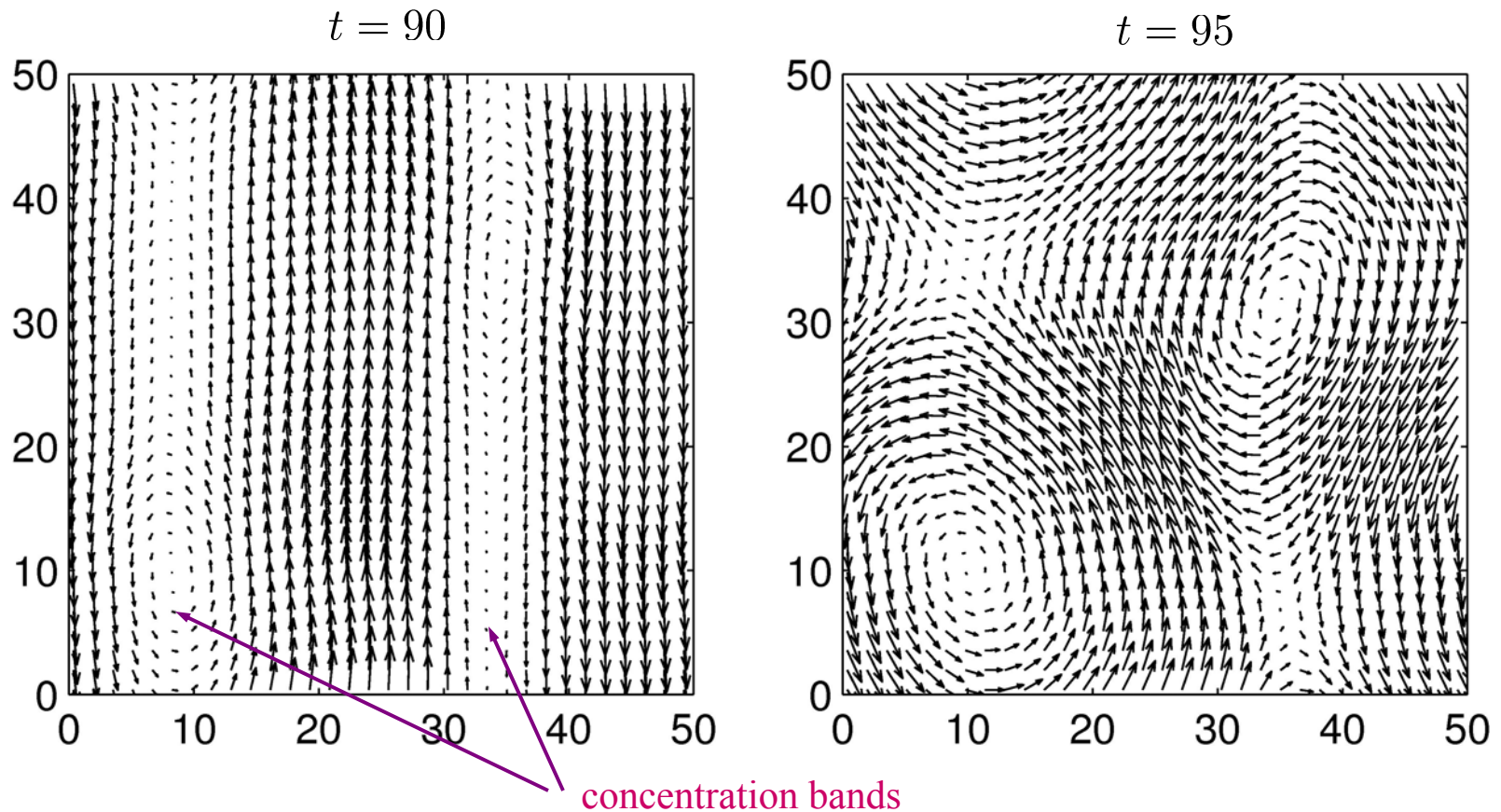
Concentration field c



Mean director field \mathbf{n}



Long-time dynamics: velocity field



- The concentration bands are located inside shear layers.
- These shear layers become unstable, leading to the formation of vortices and to the break-up of the bands, which then reform in the transverse direction.

Configurational entropy:
$$\left\{ \begin{array}{l} S = \int dV_x \int dS_p \left(\frac{\Psi}{\Psi_0} \right) \ln \left(\frac{\Psi}{\Psi_0} \right) \\ \geq 0; =0 \text{ only for } \Psi \equiv \Psi_0 \end{array} \right.$$

$$\Rightarrow \frac{dS}{dt} = \frac{3}{\alpha \Psi_0} \int dV_x \mathbf{E} : \boldsymbol{\Sigma}^a - \frac{1}{\Psi_0} \int dV_x \int dS_p \Psi \left[D |\nabla_x \ln \Psi|^2 + d |\nabla_p \ln \Psi|^2 \right]$$

But ... from the momentum equations:

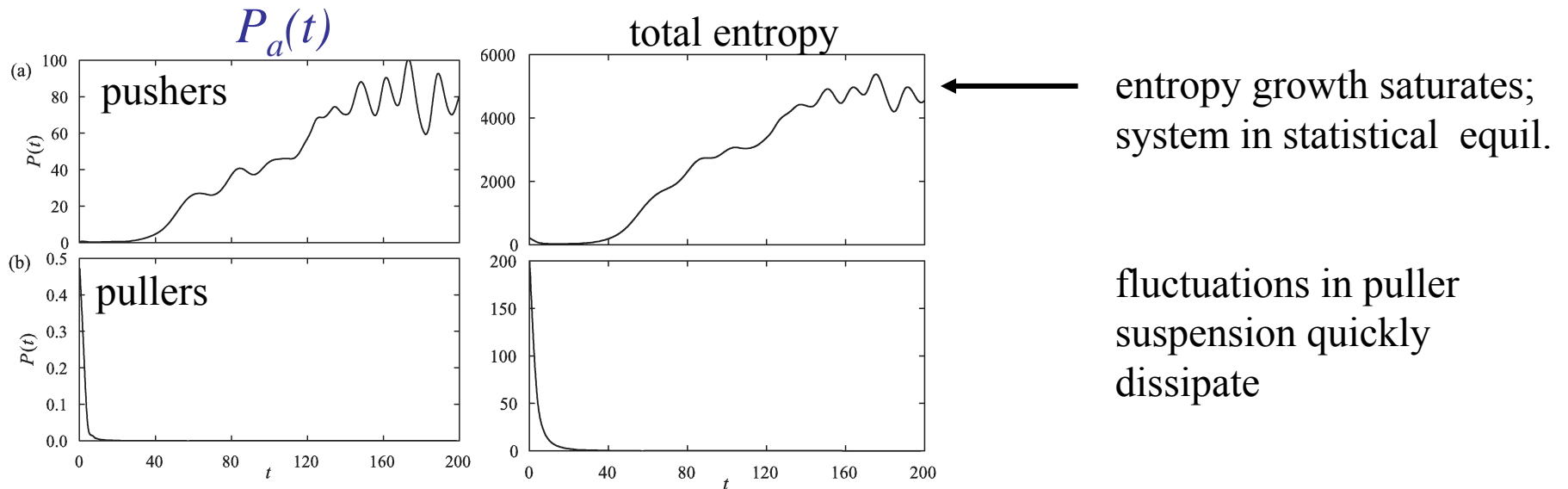
$$P_a(t) = - \int dV_x \mathbf{E} : \boldsymbol{\Sigma}^a = 2 \int dV_x \mathbf{E} : \mathbf{E}$$

rate of viscous dissipation balances the active power input $P_a(t)$ of the swimmers

$$\Rightarrow \frac{dS}{dt} = \frac{-6}{\alpha \Psi_0} \int dV_x |\mathbf{E}|^2 - \frac{1}{\Psi_0} \int dV_x \int dS_p \Psi \left[D |\nabla_x \ln \Psi|^2 + d |\nabla_p \ln \Psi|^2 \right]$$

Pullers ($\alpha > 0$): fluctuations, as measured by S , will dissipate.

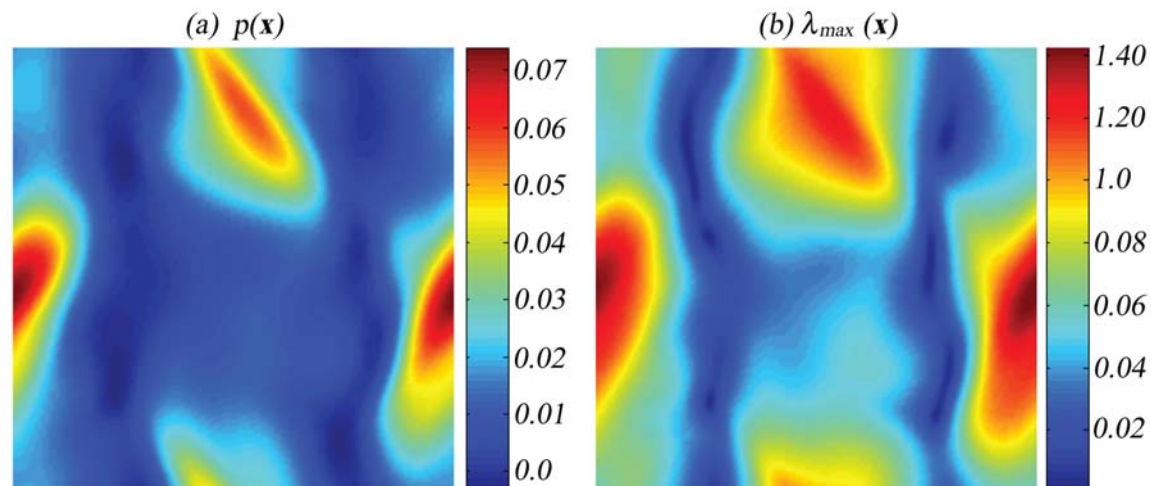
Pushers ($\alpha < 0$): the input power increases fluctuations, until limited by diffusive processes.



Active swimmer power density:

$$p(\mathbf{x}, t) = - \int dp (\alpha \mathbf{p}^T \mathbf{E}(\mathbf{x}, t) \mathbf{p}) \Psi(\mathbf{x}, \mathbf{p}, t); \quad P_a(t) = \int dV_x p(\mathbf{x}, t)$$

For $P_a(t)$ to be positive w. $\alpha < 0$, expect \mathbf{p} to be aligned with extensional axis of \mathbf{E}



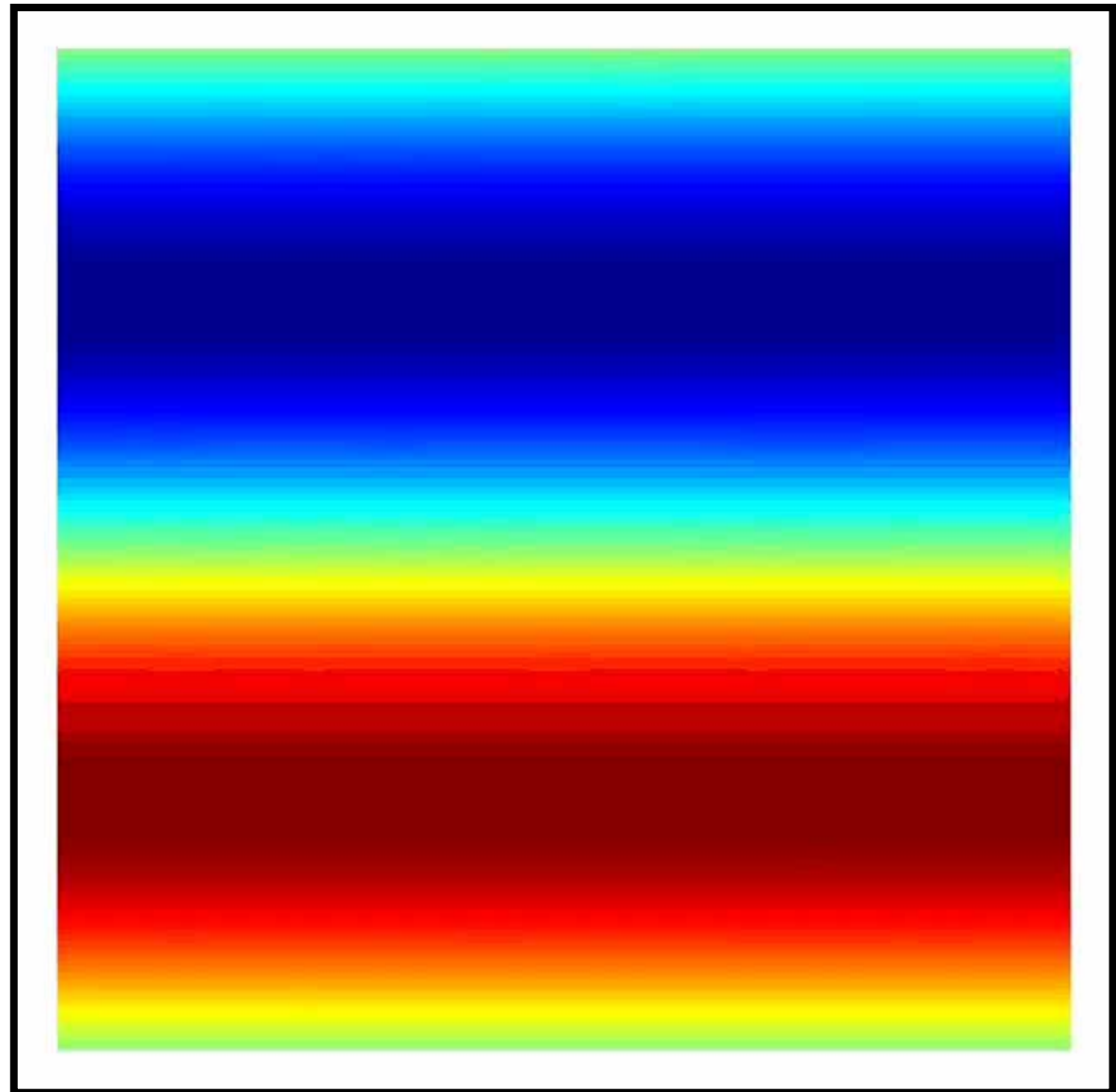
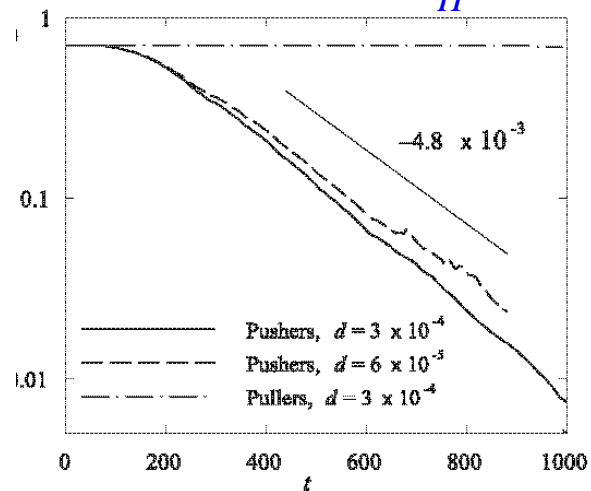
Mixing by active suspensions

Efficient convective fluid mixing is achieved by stretching and folding of fluid elements during the formation and break-up of the concentration bands.

After approximately 4 cycles, good mixing is achieved in the suspension.

From Mathew *et al* '07:

mixing norm": $\|s\|_{H^{-1/2}}$



Conclusions

- **Aligned suspensions of swimming rods destabilize as a result of hydrodynamic interactions.**
- **The chaotic flow fields arising in suspensions of swimming rods are dominated locally by near uniaxial extensional (pushers) and compressional (pullers) flows.**
- **At steady state, particle orientations show a clear correlation at short length scales owing to the disturbance flow and to hydrodynamic interactions. This correlation results in an enhancement (or decrease) of the mean particle swimming speed.**
- **Dynamics in thin liquid films are characterized by a strong particle migration towards the gas/liquid interfaces.**

- **Kinetic theory predicts instabilities for both aligned and isotropic suspensions. In the isotropic case, the instability is driven by the particle shear stress.**
- **Non-linear simulations show that active suspensions evolve toward non-uniform distributions as a result of these instabilities. More precisely, the shear stress instability causes the local polar alignment of the particles, which in turn results in the formation of concentration inhomogeneities.**