

Near-surface ion distribution and buffer effects during electrochemical reactions

MIR@W day: Modelling and simulation
of electrochemical flows in Lithium-ion
batteries

Dr. Michael AUINGER

MIR@W day

Zeeman Building, University of Warwick
Coventry CV4 7AL, United Kingdom

30th November, 2015





The Beauty of Thermochemical Simulations

MIR@W day: Modelling and simulation of electrochemical flows in Lithium-ion batteries

Dr. Michael AUINGER

MIR@W day
Zeeman Building, University of Warwick
Coventry CV4 7AL, United Kingdom
30th November, 2015

The Steels Processing Group



Prof. S. Seetharaman
Physical Metallurgy



C. Davis
Mechanics



B. Shollock
Coatings



R. Dashwood
Director



P. Srirangam
in-situ

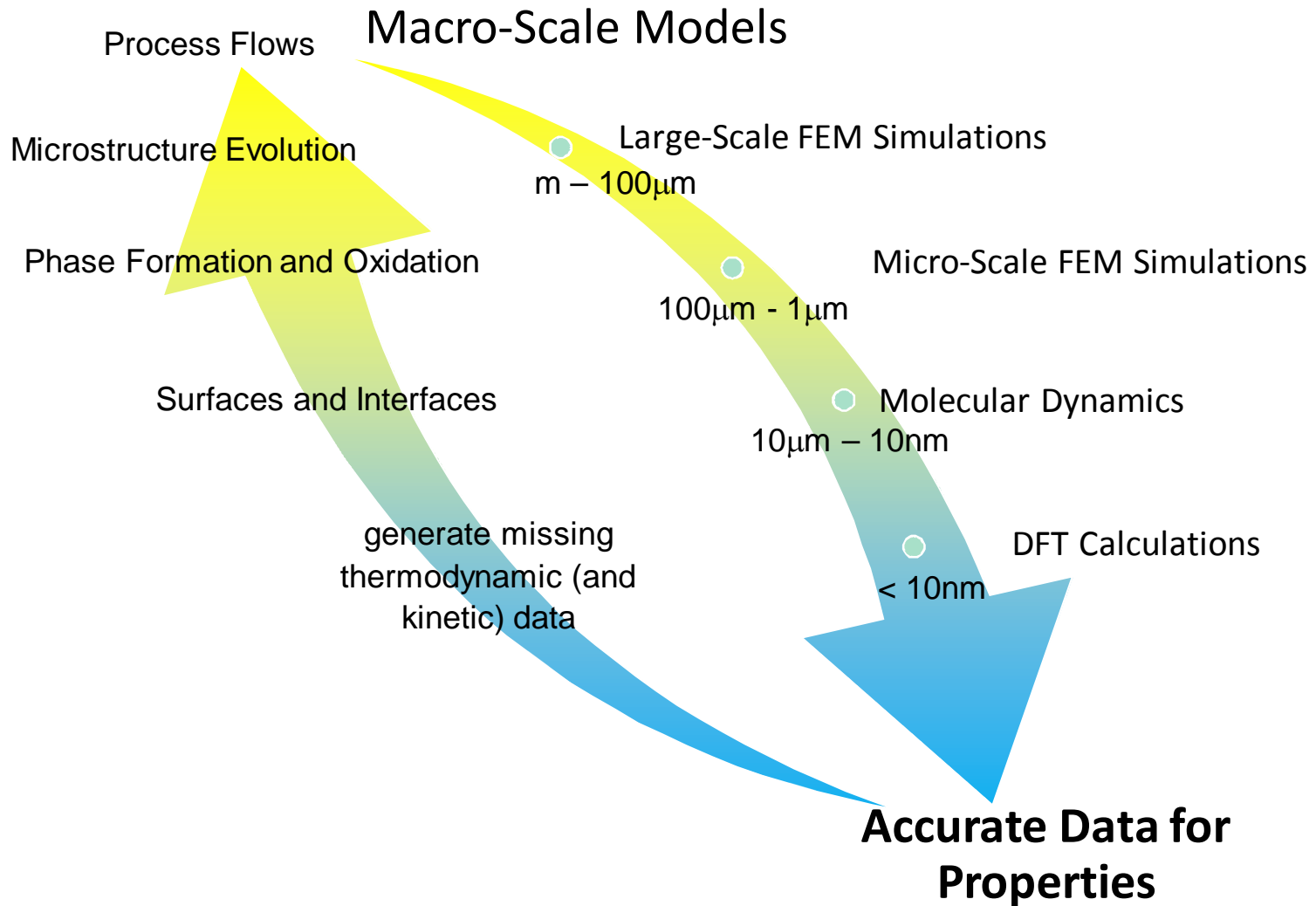


R. Bhagat
EChem.



M. Auinger
Modelling

The Hierarchy of Modelling



Theoretical Model and Discussion

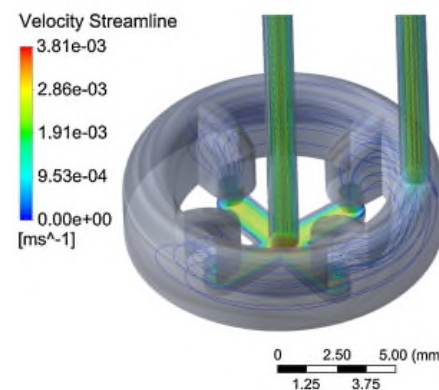
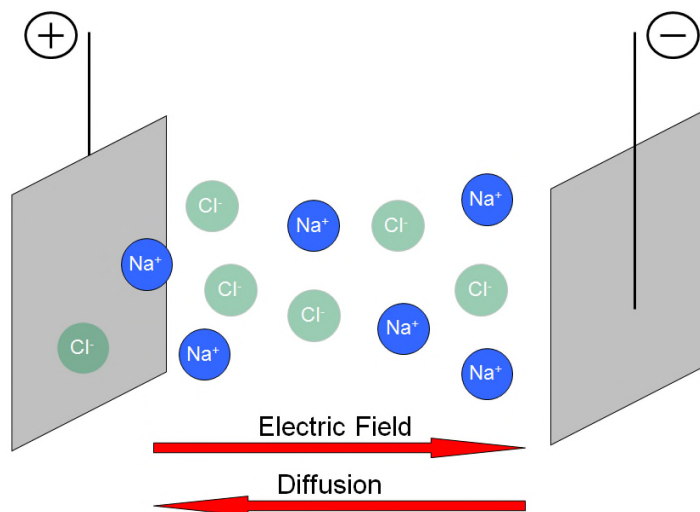
$$\left\{ \frac{\partial c_i}{\partial t} = \text{div} \left(D_i \nabla c_i + \frac{D_i z_i e_0}{k_B T} c_i \nabla \varphi + c_i v_i \right) \right\} \quad (i = A, B, C, D)$$

ion diffusion

migration in an electric field

$$K = \frac{c_C c_D}{c_A c_B}$$

chemical equilibrium



convection

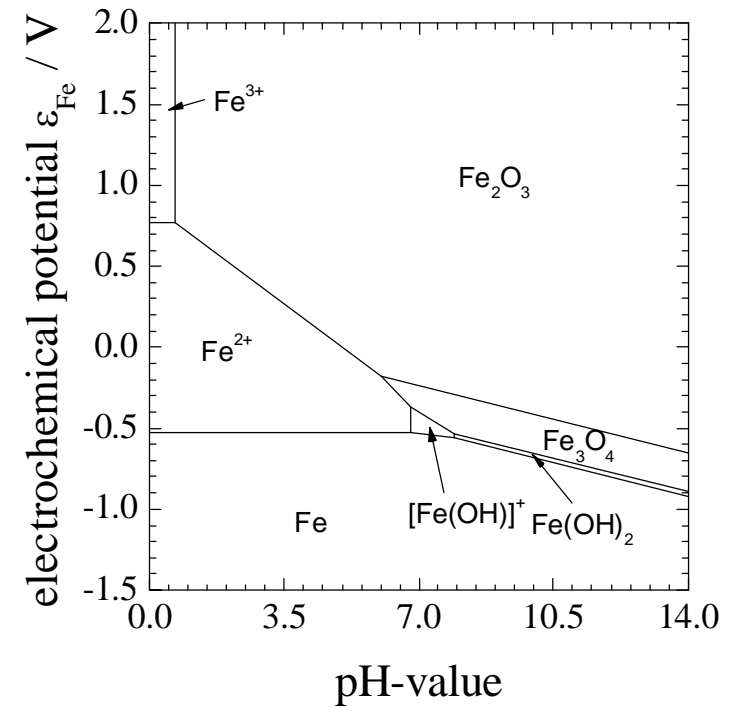
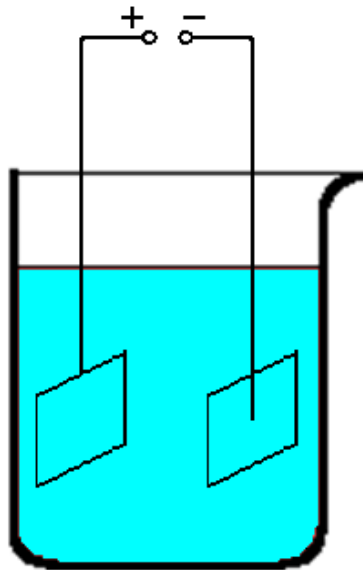
P. Skladal, *Analytica Chimica Acta*
727 (2012) 41–46.

element transport

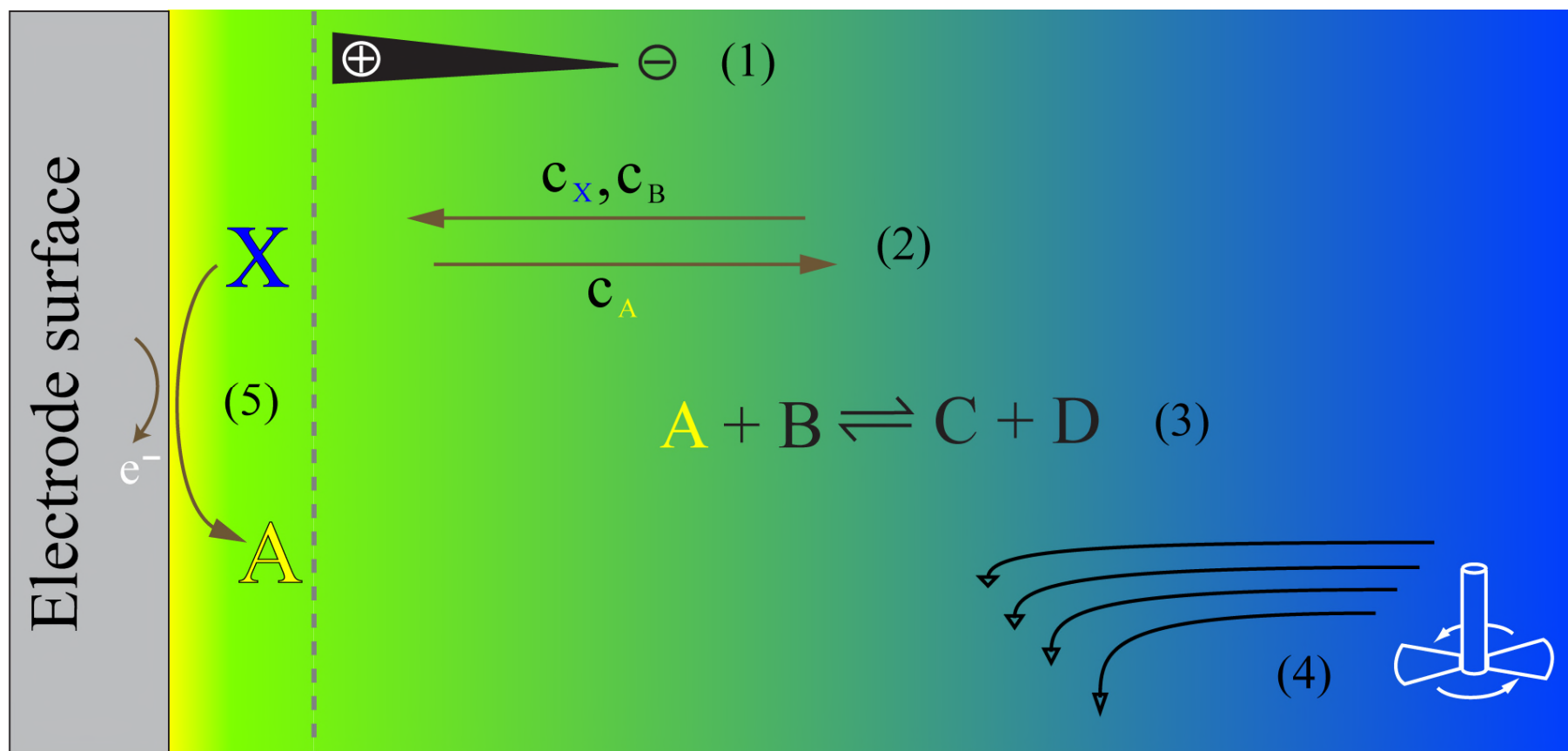
chemical reaction

$$\frac{dc_{i(x,t)}}{dt} = \text{div}(D_{i(x,T)} \cdot \nabla c_{i(x,t)} + z_i \cdot \mu_{i(x,T)} \cdot c_{i(x,t)} \cdot \nabla \phi_{(x,t)})$$

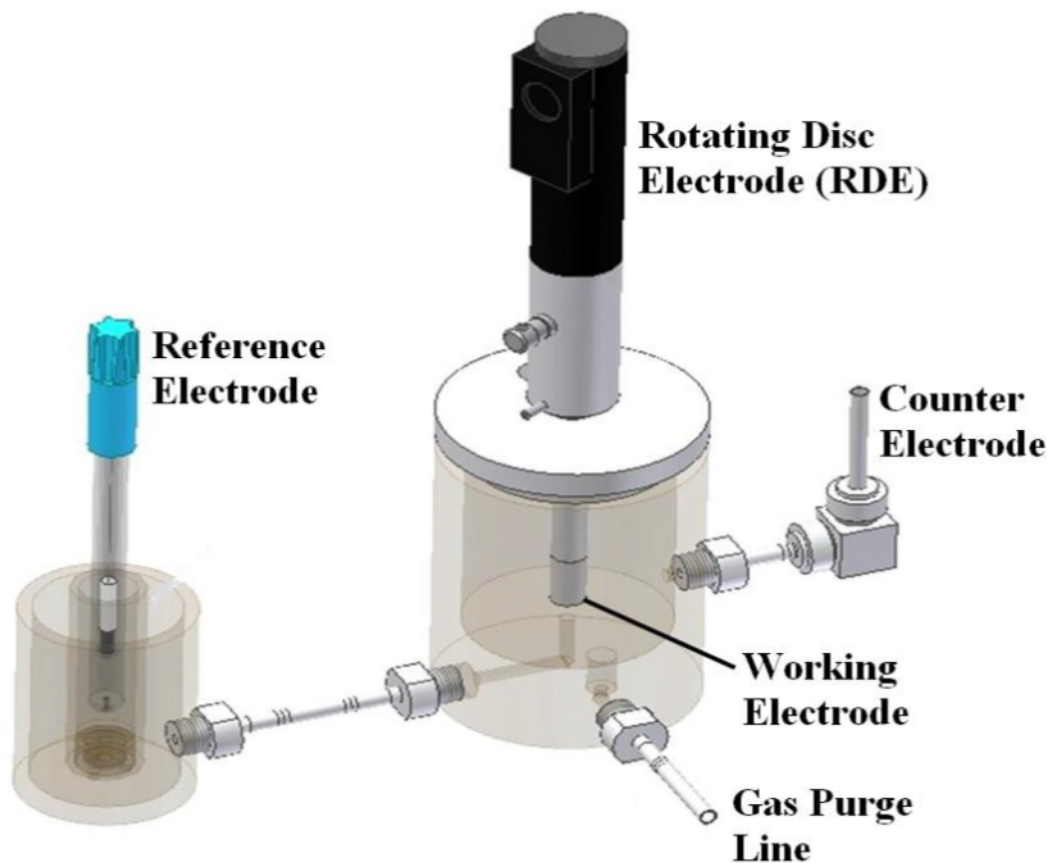
CHEMAPP



Electrochemistry & surface pH-values



Experimental RDE-Setup



Working electrode:
polycrystalline Pt disc
(0.196 cm²), embedded in Teflon

Counter electrode:
graphite rod

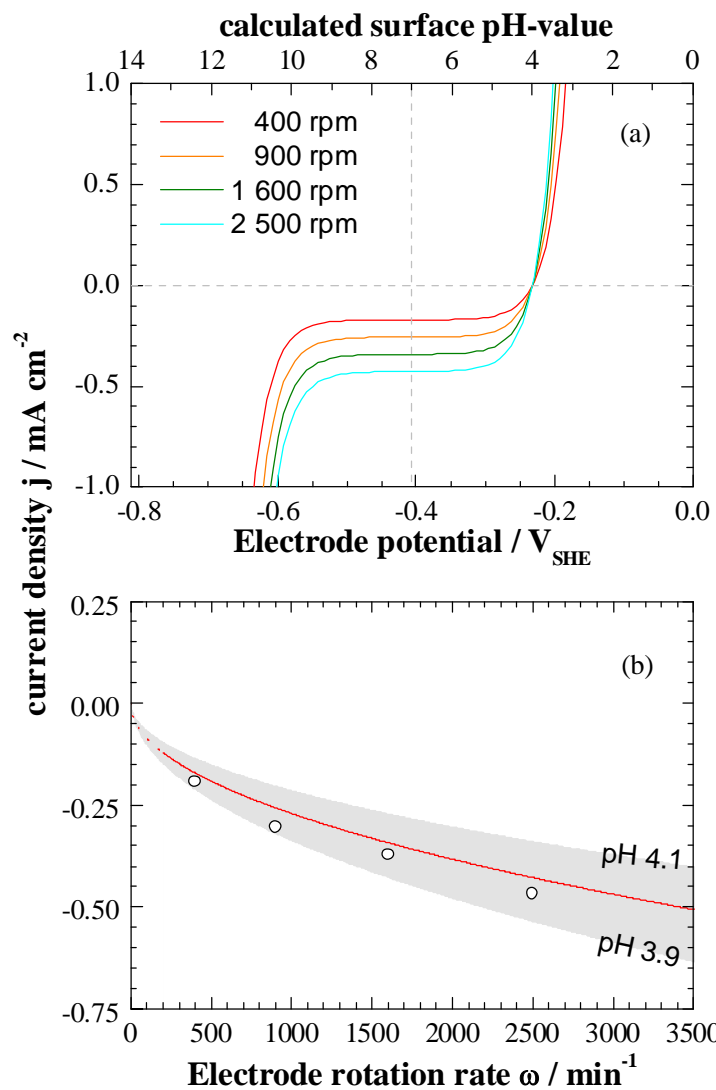
Reference electrode:
saturated Ag/AgCl

50ml Teflon 3-compartment cell

Uncompensated resistance < 2Ω

parameters controlled via
LabVIEW

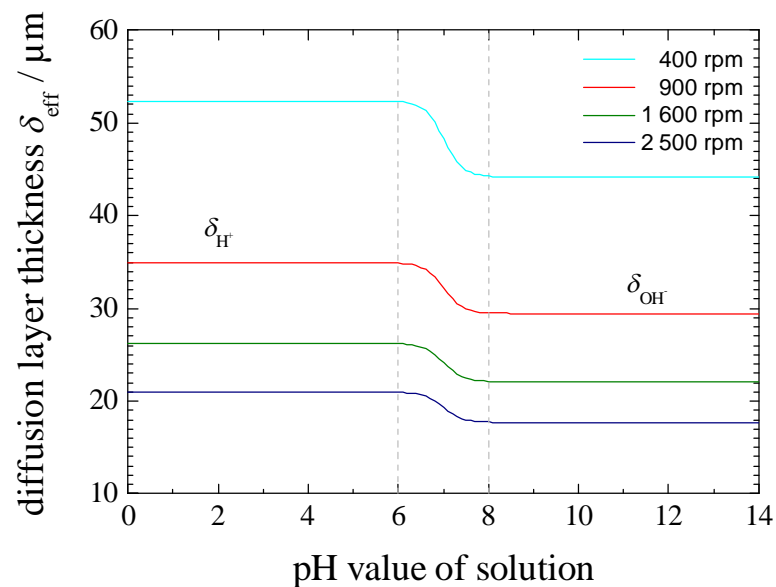
Parameters and Diffusion Layer



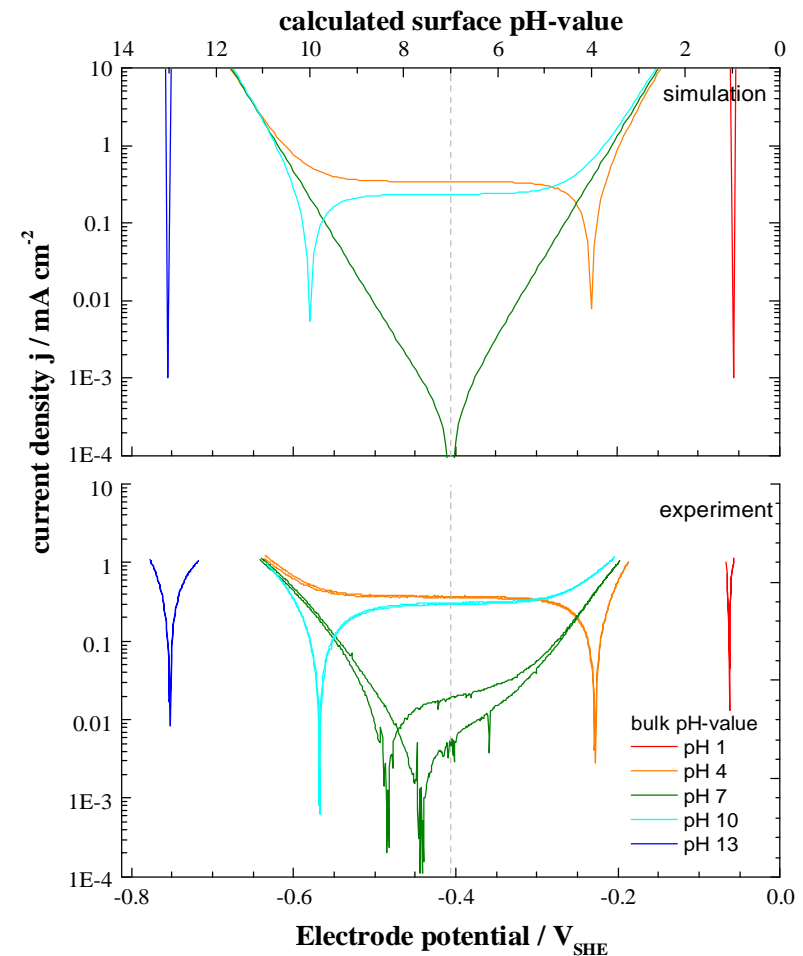
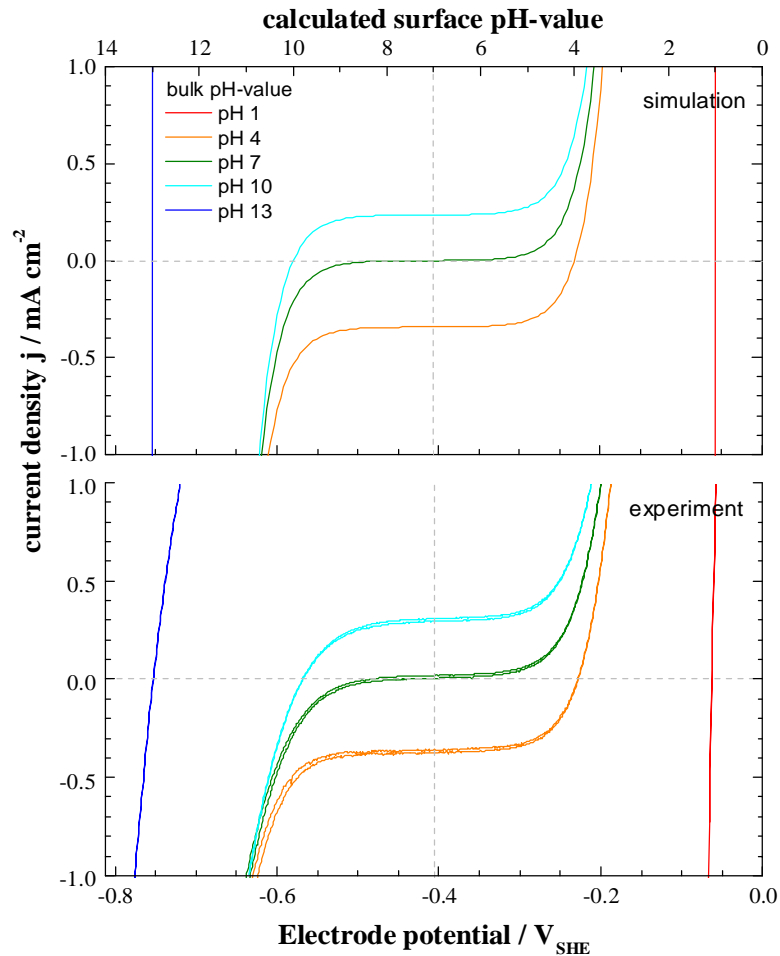
Levich Equation:

$$\delta_i = 1.6126 D_i^{\frac{1}{3}} \nu^{\frac{1}{6}} \omega^{-\frac{1}{2}}$$

$$\delta_{\text{eff}} = \frac{c_{\text{H}^+} \delta_{\text{H}^+} + c_{\text{OH}^-} \delta_{\text{OH}^-}}{c_{\text{H}^+} + c_{\text{OH}^-}}$$



Unbuffered Aqueous Solution



unbuffered solution:

$$j_{H^+/OH^-} = \frac{F}{\delta_{eff}} \left[D_{H^+} (c_H^{surface} - c_H^{solution}) - D_{OH^-} K_w \left(\frac{1}{c_H^{surface}} - \frac{1}{c_H^{solution}} \right) \right]$$

Local Corrosion Effects

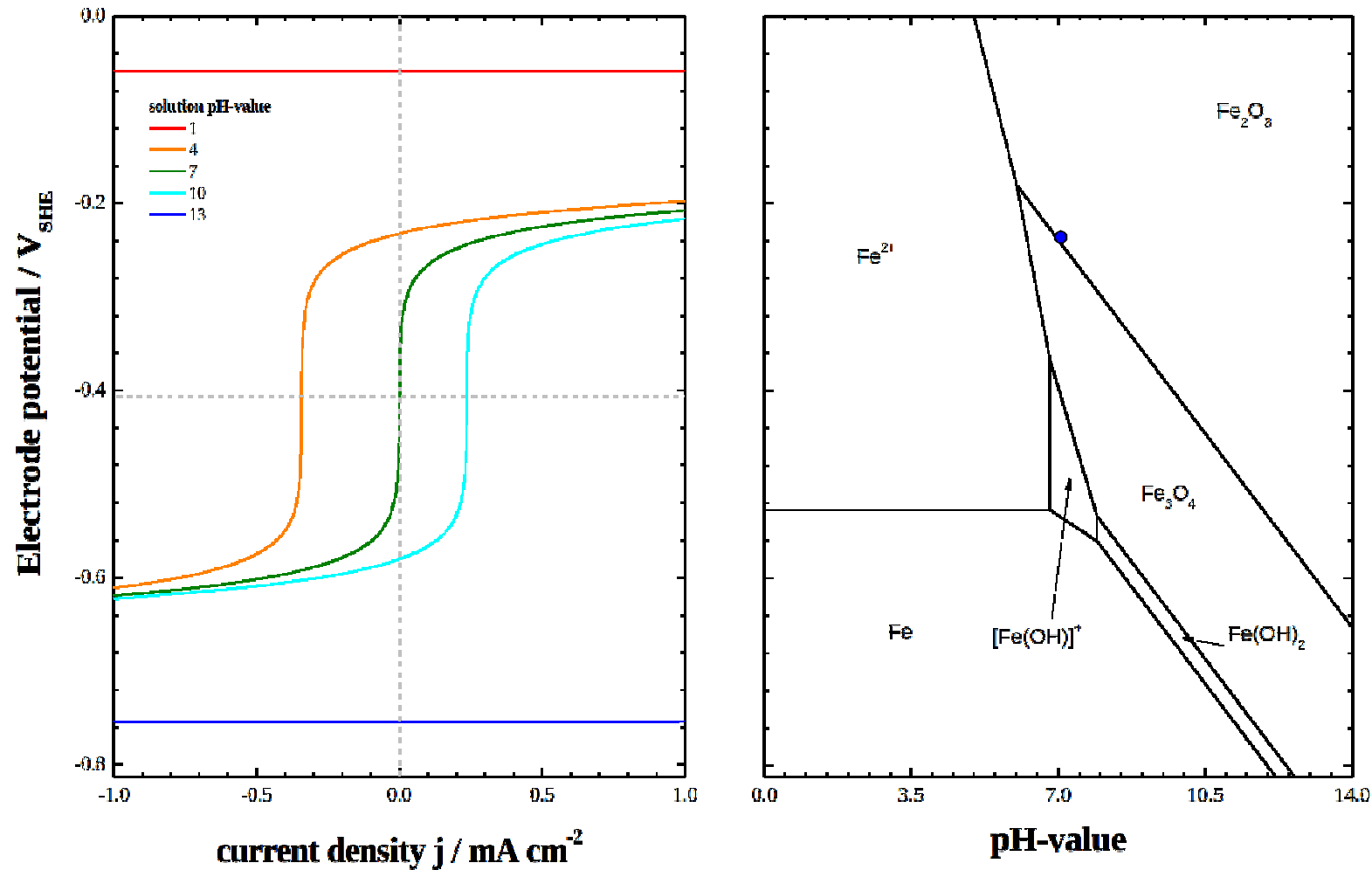


Figure: Cyclic voltammograms in unbuffered solutions of different pH-value.

Local Corrosion Effects

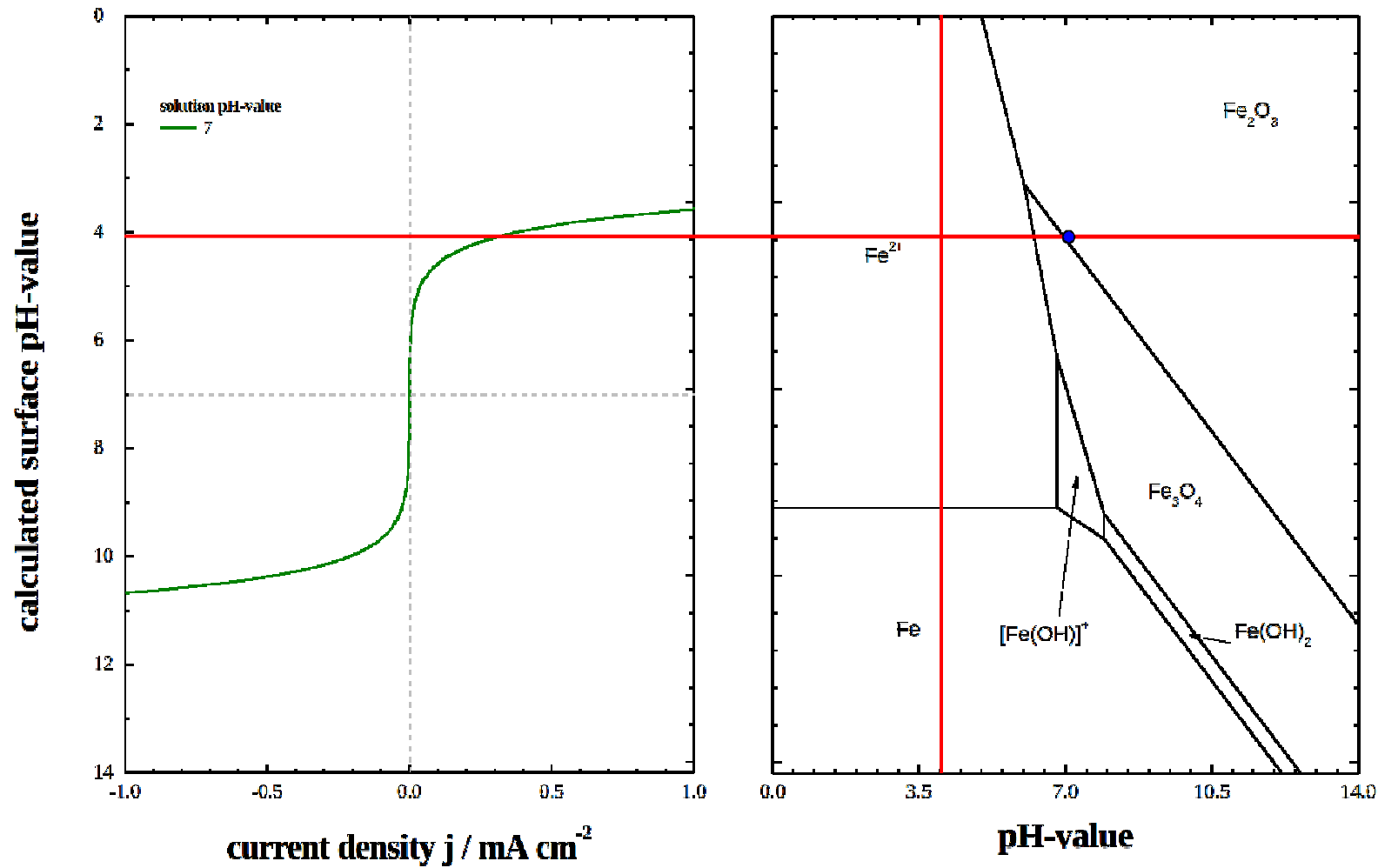


Figure: Cyclic voltammograms in unbuffered solution of pH 7.

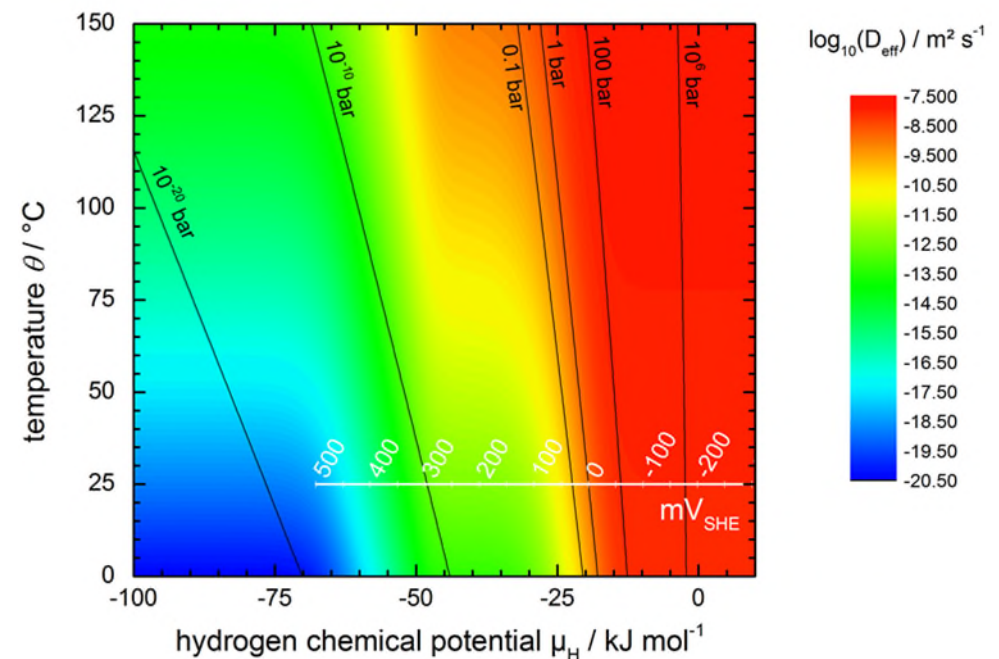
Electrochemistry & Pickling

$$\text{Nernst Equation} \quad E = E^{\circ} + \frac{RT}{zF} \ln \left(\frac{a_{Ox}}{a_{Red}} \right)$$

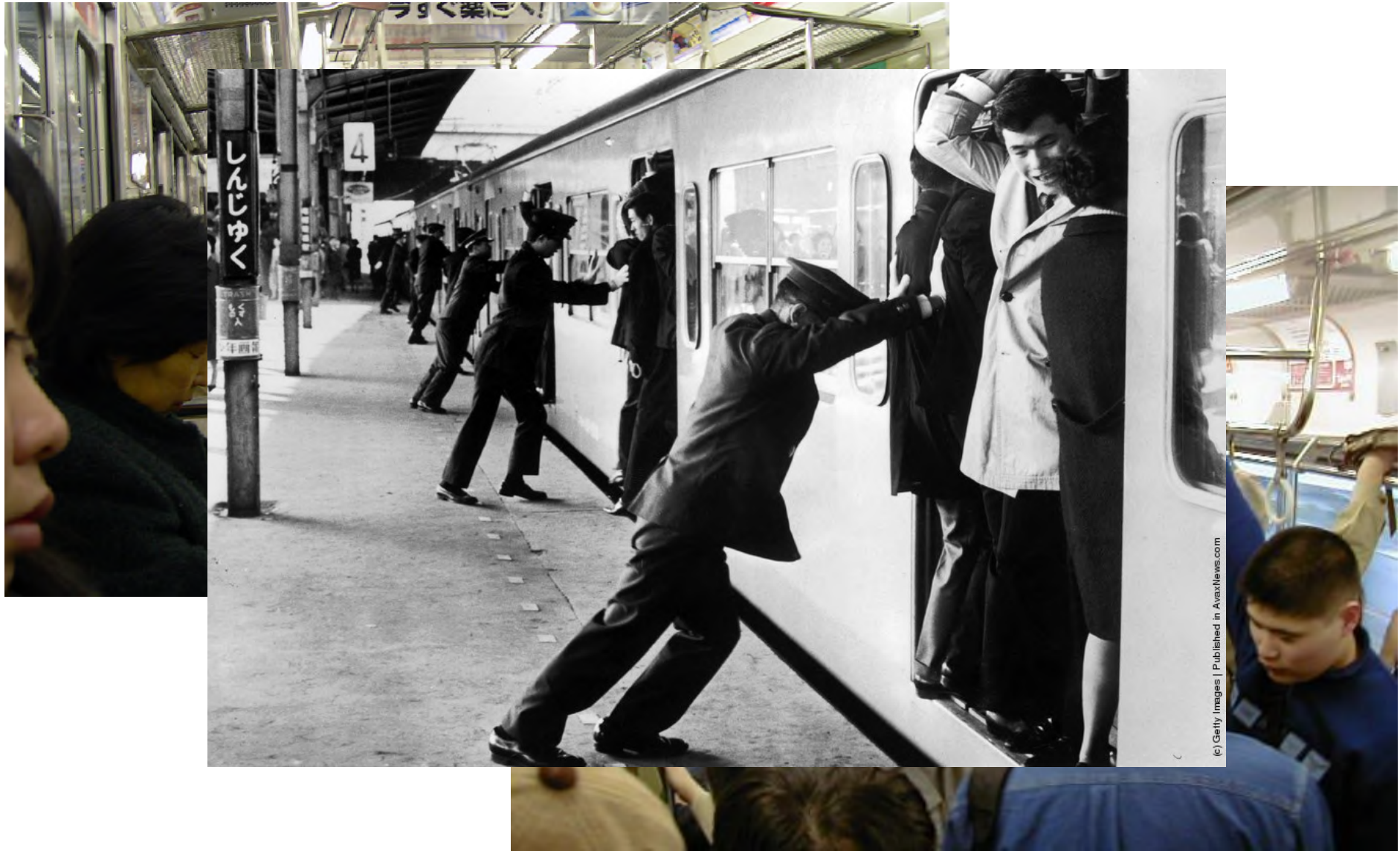
$$E = -58\text{mV pH} - (29\text{mV} \log(p(H_2)))$$

An applied voltage of -58 mV
(vs SHE) corresponds to:

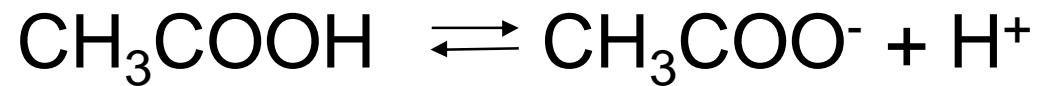
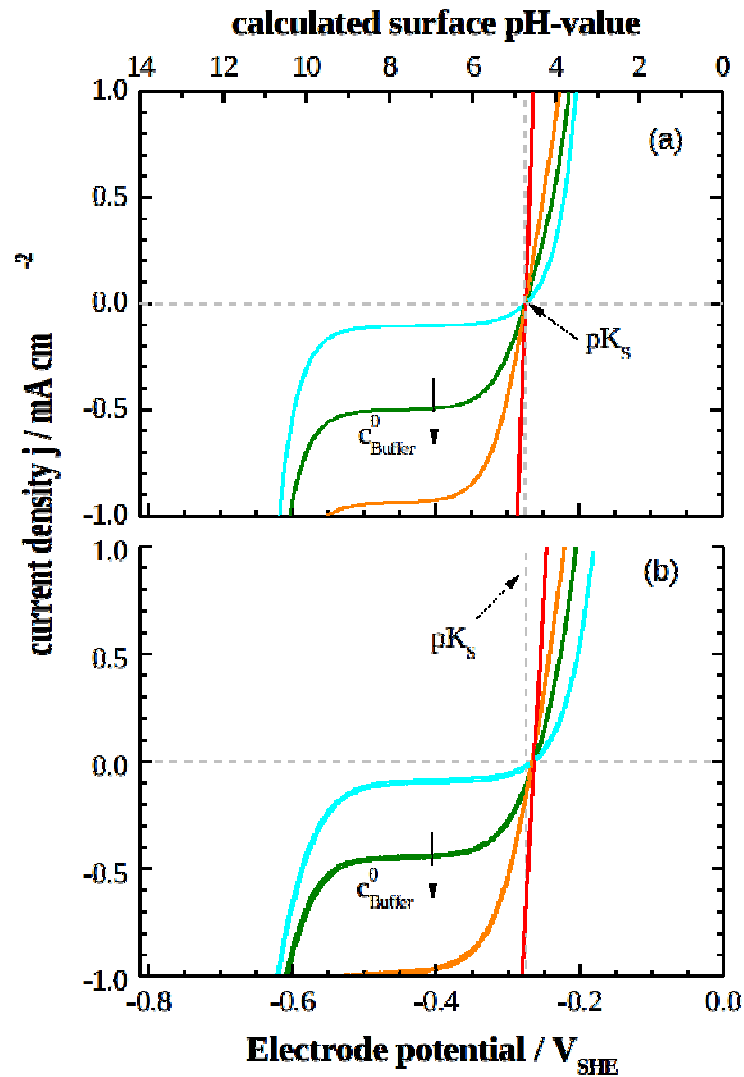
pH =	7 and	10^{-12} bar H_2
pH =	5 and	10^{-8} bar H_2
pH =	1 and	1 bar H_2
pH =	0 and	100 bar H_2



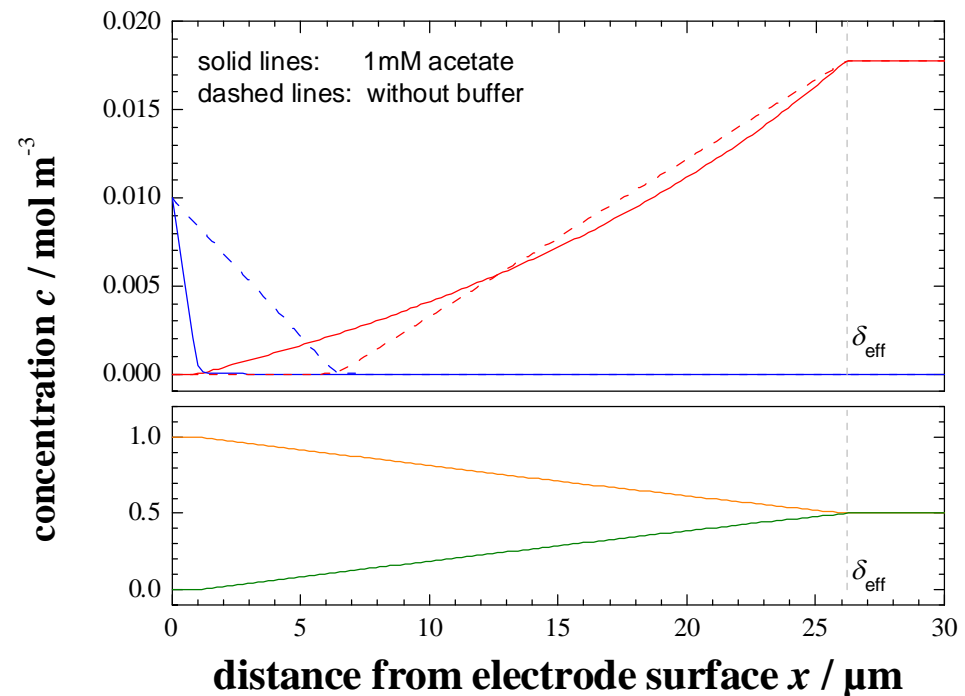
“Solubility” at extreme Conditions



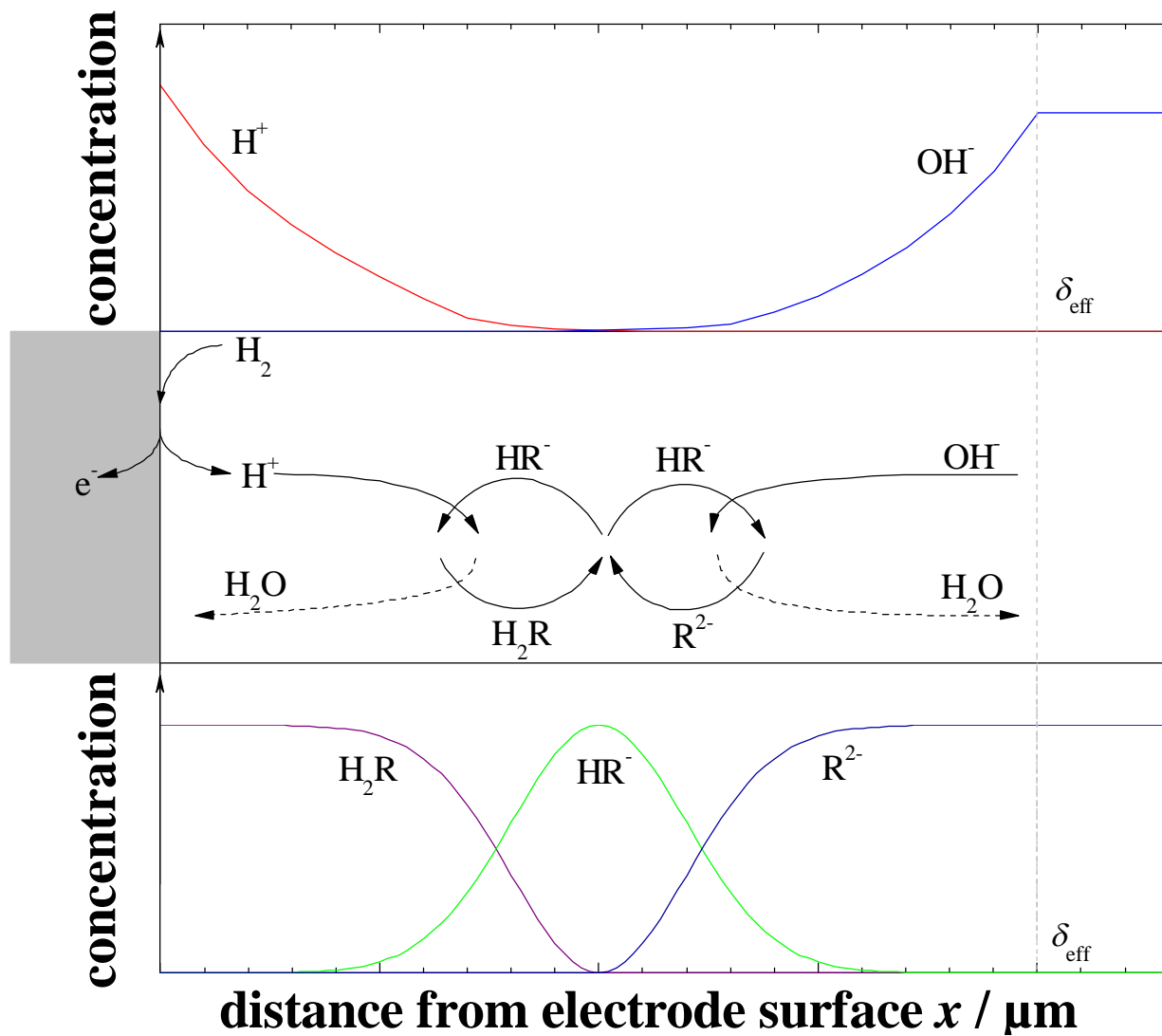
Acetate Buffered Solution



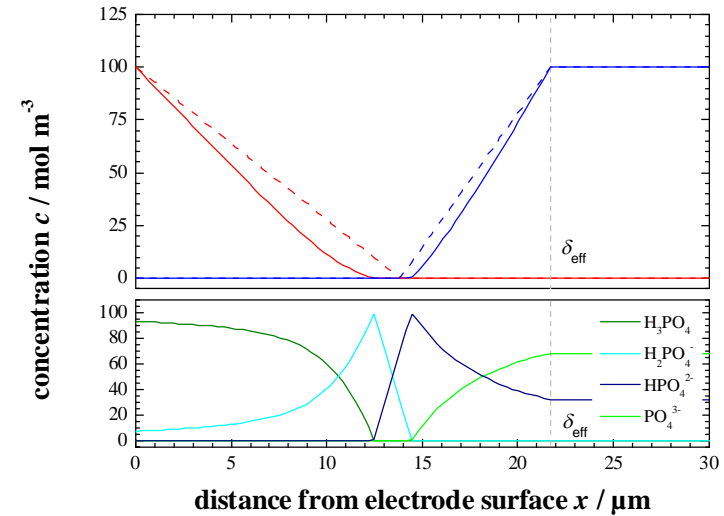
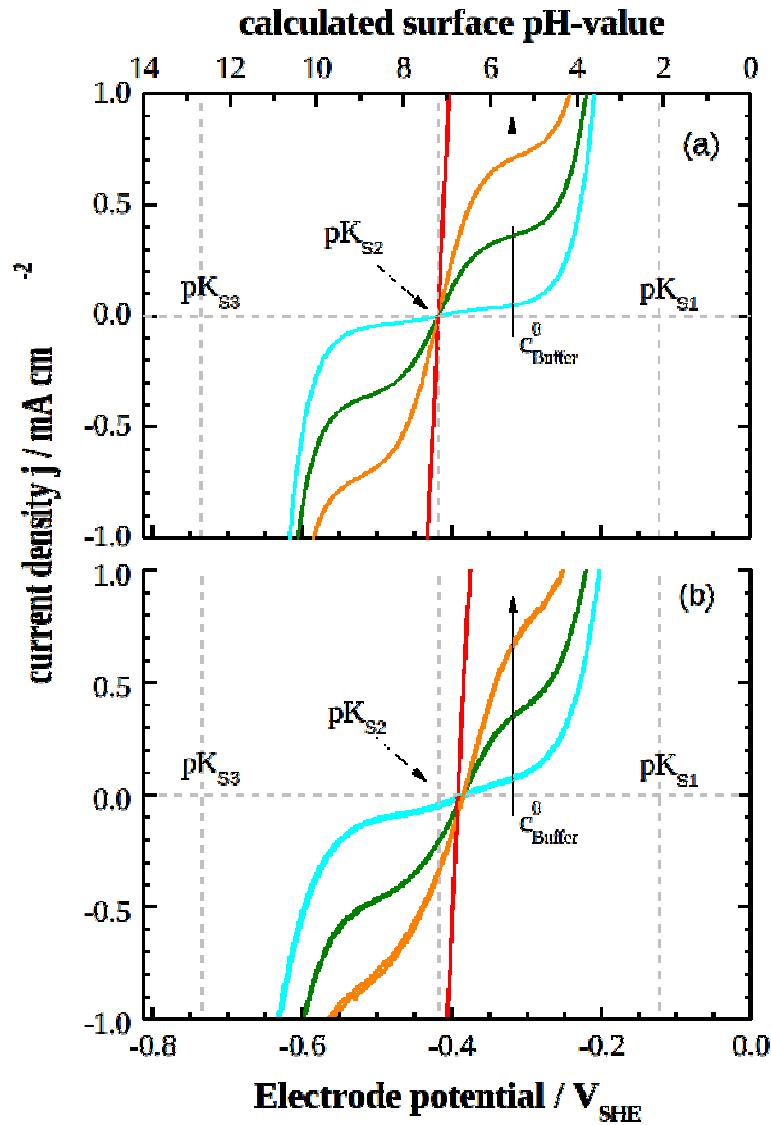
$$j = j_{\text{H}^+/\text{OH}^-} + \frac{c_{\text{Buffer}}^0 F}{\delta_{\text{eff}}} \left[\frac{D_{\text{HAc}} c_{\text{H}}^{\text{surface}} - D_{\text{Ac}} K_s}{K_s + c_{\text{H}}^{\text{surface}}} - \frac{D_{\text{HAc}} c_{\text{H}}^{\text{solution}} - D_{\text{Ac}} K_s}{K_s + c_{\text{H}}^{\text{solution}}} \right]$$



General Transport Scheme



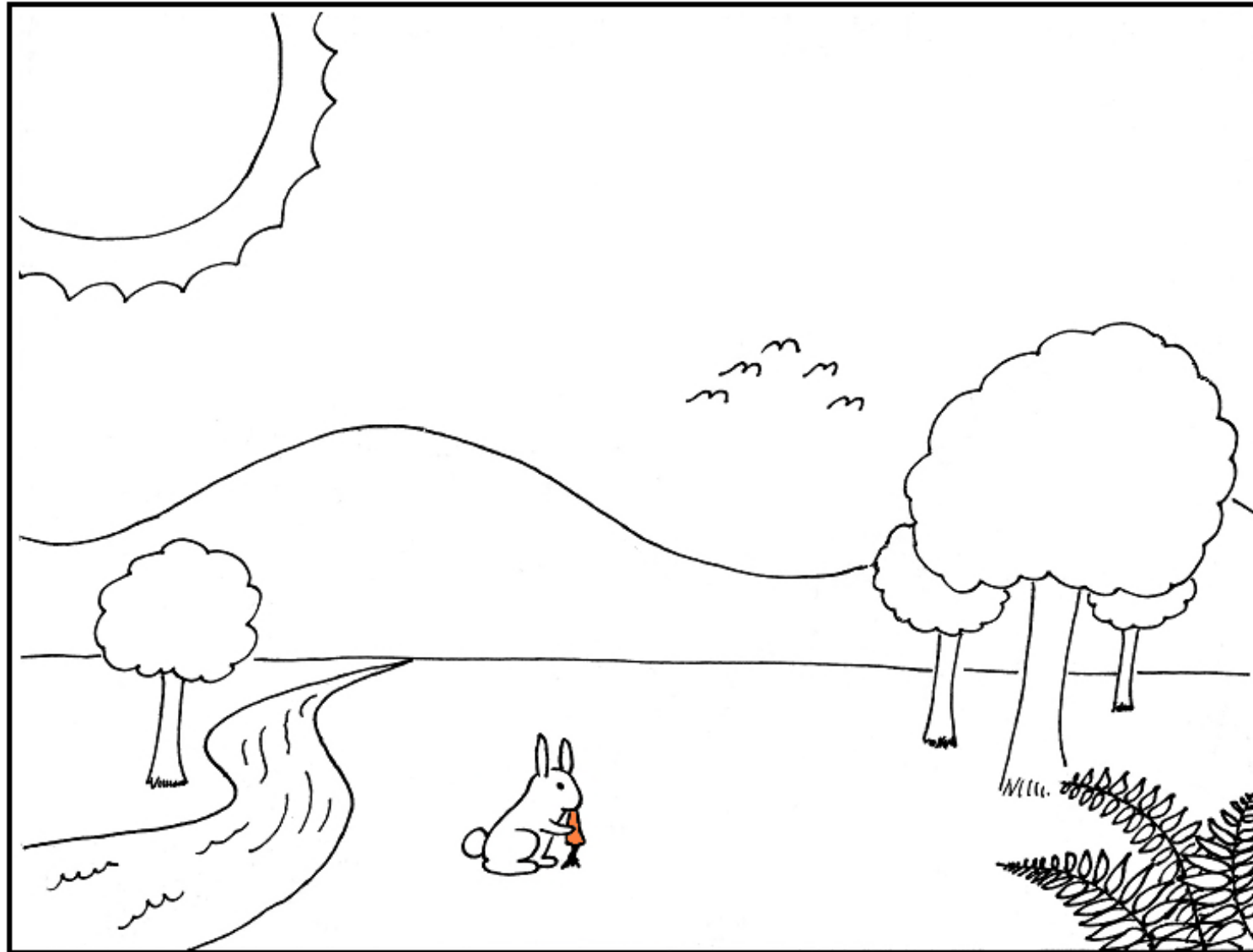
Phosphate Buffered Solution



$$j = j_{\text{H}^+/\text{OH}^-} + j_{\text{Buffer}}$$

$$j_{\text{Buffer}} = \frac{c_{\text{Buffer}}^0 F}{\delta_{\text{eff}}} \left(\frac{3D_1 + D_2 \frac{K_{S1}}{c_{(x),\text{H}^+}} - D_3 \frac{K_{S1} K_{S2}}{c_{(x),\text{H}^+}^2} - 3D_4 \frac{K_{S1} K_{S2} K_{S3}}{c_{(x),\text{H}^+}^3}}{1 + \frac{K_{S1}}{c_{(x),\text{H}^+}} + \frac{K_{S1} K_{S2}}{c_{(x),\text{H}^+}^2} + \frac{K_{S1} K_{S2} K_{S3}}{c_{(x),\text{H}^+}^3}} \right) \Bigg|_{x=\delta_{\text{eff}}}^{x=0}$$

The Use of Mathematics



The Use of Mathematics

${}^1\text{H} + {}^1\text{H} \rightarrow {}^2\text{H} + e^+ + \nu_e$
 ${}^2\text{H} + {}^1\text{H} \rightarrow {}^3\text{He} + \gamma$
 ${}^3\text{He} + {}^3\text{He} \rightarrow {}^4\text{He} + 2{}^1\text{H}$

$\nabla \cdot \mathbf{E} = \frac{1}{\epsilon_0} \rho$
 $\nabla \cdot \mathbf{B} = 0$
 $\nabla \times \mathbf{E} + \frac{\partial \mathbf{B}}{\partial t} = 0$
 $\nabla \times \mathbf{B} = \mu_0 \mathbf{J} + \mu_0 \epsilon_0 \frac{\partial \mathbf{E}}{\partial t}$

$F = G \frac{m_1 m_2}{r^2}$
 $R_{\mu\nu} - \frac{1}{2} R g_{\mu\nu} = 8\pi G T_{\mu\nu}$

$f(x) = a_0 + \sum_{n=1}^{\infty} (a_n \cos nx + b_n \sin nx)$

$P + \frac{1}{2} \rho v^2 + \rho gh = C$
 $n\text{CO}_2 + n\text{H}_2\text{O} \xrightarrow{h\nu} (\text{CH}_2\text{O})_n + n\text{O}_2$
 $\text{CO}_2 \rightarrow \text{O}_2$

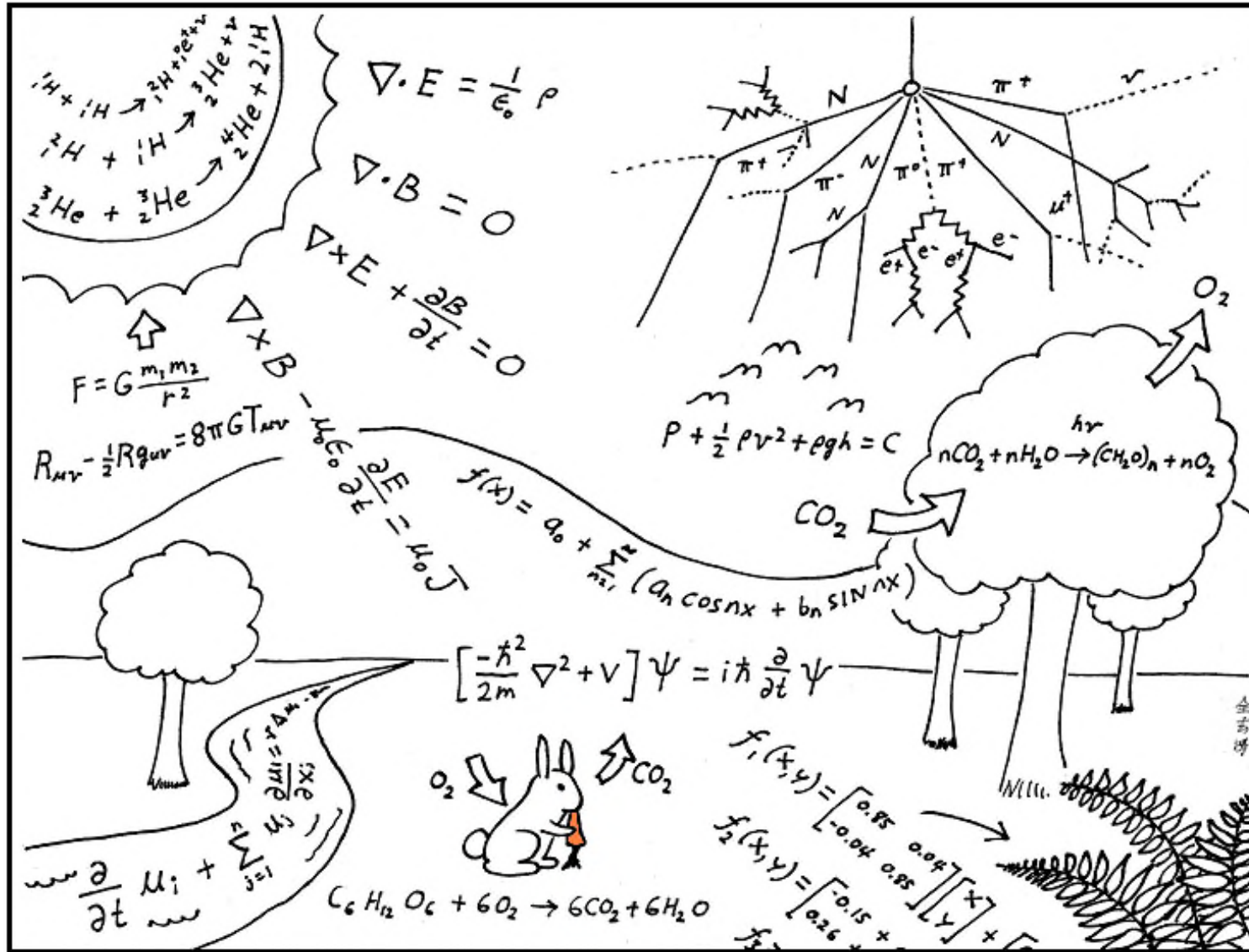
$[\frac{-\hbar^2}{2m} \nabla^2 + V] \psi = i\hbar \frac{\partial}{\partial t} \psi$

$\frac{\partial}{\partial t} \mu_i + \sum_{j=1}^n \frac{\partial \mu_j}{\partial x} \frac{\partial x_j}{\partial x} = \frac{\partial \mu}{\partial x}$

$C_6H_{12}O_6 + 6O_2 \rightarrow 6CO_2 + 6H_2O$

$f_1(x,y) = \begin{bmatrix} 0.15 & 0.04 \\ -0.04 & 0.15 \end{bmatrix} \begin{bmatrix} x \\ y \end{bmatrix} + \begin{bmatrix} 1.7 \\ 1.9 \end{bmatrix}$
 $f_2(x,y) = \begin{bmatrix} -0.15 & 0.04 \\ 0.04 & -0.15 \end{bmatrix} \begin{bmatrix} x \\ y \end{bmatrix} + \begin{bmatrix} -1.7 \\ -1.9 \end{bmatrix}$

The Use of Mathematics

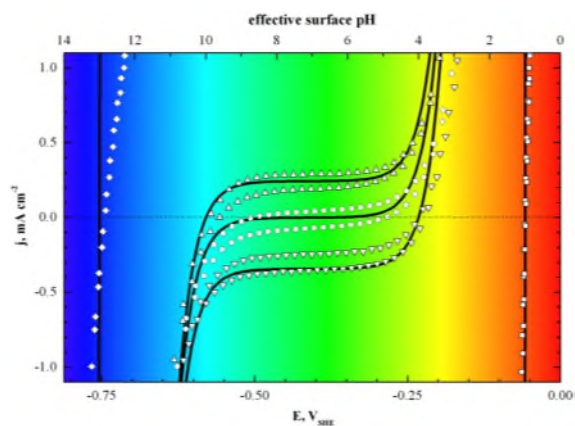
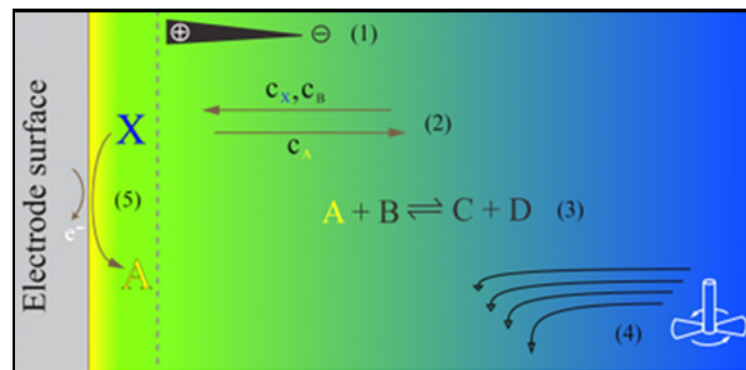


Summary

Near-surface ion distribution and buffer effects during electrochemical reaction

M. Auinger, I. Katsounaros, J.C. Meier, S.O. Klemm, P.U. Biedermann, A.A. Topalov, M. Rowherder, K.J.J. Mayrhofer

PCCP 13 (2011) 16384-16394.



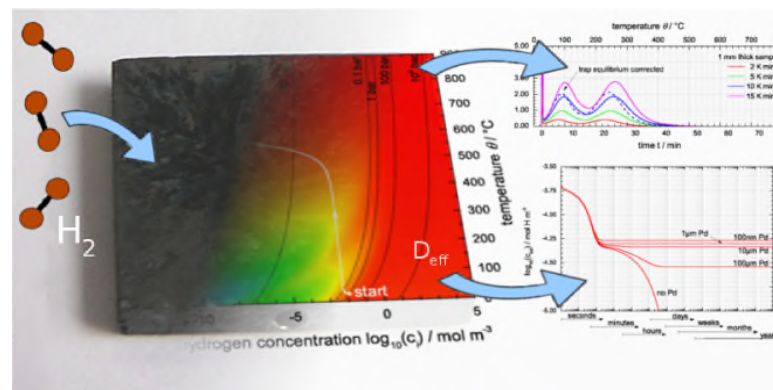
The effective surface pH during reactions at the solid-liquid interface

I. Katsounaros, J.C. Meier, S.O. Klemm, A.A. Topalov, P.U. Biedermann, M. Auinger, K.J.J. Mayrhofer

Electrochem. Commun. 13 (2011) 634-637.

Hydrogen Transport in non-ideal Crystalline Materials

M. Auinger, Chem. Phys. Chem. 15 (2014) 2893-2902.



Acknowledgement

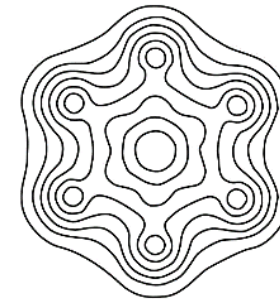


Max-Planck-Institut
für Eisenforschung GmbH

K. Mayrhofer, J.C. Meier, A.A. Topalov, I. Katsounaros,
D. Kurz, A. Mingers



Christian Doppler
Forschungsgesellschaft



FCI
FONDS DER
CHEMISCHEN
INDUSTRIE

voestalpine

EINEN SCHRITT VORAUS.

